

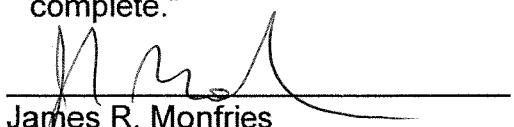


SOURCE EMISSIONS SURVEY
OF
CITGO PETROLEUM CORP.
FCCU WESP STACK
LEMONT, ILLINOIS

JUNE AND JULY 2010

TESTING COMPANY: METCO ENVIRONMENTAL
P.O. BOX 598
ADDISON, TEXAS 75001
972-931-7127
FILE NUMBER 10-274B

" I certify that I have personally checked and am familiar with the information submitted herein, and based on my inquiries of those individuals immediately responsible for obtaining the information, I believe the submitted information is true, accurate, and complete."


James R. Monfries
Senior Quality Assurance Manager

*File Number 10-274B*

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SOURCE EMISSIONS SURVEY
CITGO PETROLEUM CORP.
FCCU WESP STACK
LEMONT, ILLINOIS
FILE NUMBER 10-274B

INTRODUCTION

METCO Environmental, P.O. Box 598, Addison, Texas, conducted a source emissions survey of CITGO Petroleum Corp., located in Lemont, Illinois, on June 29 through July 1, 2010. The purpose of these tests was to determine the concentrations of particulate matter being emitted to the atmosphere via the FCCU WESP Stack. The testing was performed while the unit was operating at an average coke burn rate of 61,324 lbs/hr.

The sampling was performed by the following METCO personnel: John Cutaia – Project Supervisor, Kyle Gilbert, Will Starkey, Sam Morris, and Landon Bippert.

The sampling followed the procedures set forth in the Code of Federal Regulations, Title 40, Chapter I, Part 60, Appendix A, Methods 1, 2, 3B, 4, and 5B.



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SUMMARY OF RESULTS

FCCU WESP Stack

<u>Run Number</u>	<u>"Front-Half"</u>		
	<u>Non-Sulfuric Acid Particulate Matter</u>	<u>(gr/dscf*)</u>	<u>(lbs/hr)</u>
1A	0.0415	90.19	1.46
1B	0.0525	106.19	1.72
2A	0.0320	68.48	1.48
2B	0.0436	90.41	1.12
3A	0.0191	40.83	0.67
3B	<u>0.0190</u>	<u>38.78</u>	<u>0.64</u>
Average	0.0345	72.31	1.18
Allowable Emission Rate	---	---	≤ 1.0

*29.92" Hg, 68°F (760 mm Hg, 20°C)


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SUMMARY OF RESULTS

FCCU WESP Stack

"Method 5B/202"

Run Number	1A	2A	3A
Date	06/30/10	07/01/10	07/01/10
Time	1908-2034	1208-1346	1500-1636
Stack Flow Rate – ACFM	374,617	374,859	374,164
Stack Flow Rate – DSCFM*	253,287	249,596	249,542
% Water Vapor - % Vol.	21.71	23.73	23.57
% CO ₂ - % Vol.	14.3	14.4	14.5
% O ₂ - % Vol.	4.2	3.6	3.7
Excess Air @ Sampling Point - %	24.1	19.9	20.6
Stack Temperature - °F	148	147	147
Stack Pressure – "Hg	29.64	29.92	29.90
Percent Isokinetic	102.2	99.3	97.9
Volume Dry Gas Sampled – DSCF*	34.284	32.804	32.342
Coke Burned – mlb	61.870	61.222	60.881
Particulates			
<u>Probe, Cyclone & Filter Catch</u> grains/dscf*	0.0415	0.0320	0.0191
grains/cf @ Stack Conditions	0.0280	0.212	0.127
lbs/hr	90.19	68.48	40.83
lb/mlb coke burned	1.46	1.12	0.67

* 29.92 "Hg, 68°F (760 mm Hg, 20°C)



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SUMMARY OF RESULTS

FCCU WESP Stack

"Method 5B/OTM-28"

Run Number	1B	2B	3B
Date	06/30/10	07/01/10	07/01/10
Time	1908-2034	1208-1346	1500-1636
Stack Flow Rate – ACFM	361,609	362,854	360,197
Stack Flow Rate – DSCFM*	235,905	242,089	238,409
% Water Vapor - % Vol.	24.32	23.45	23.89
% CO ₂ - % Vol.	14.3	14.4	14.5
% O ₂ - % Vol.	4.2	3.6	3.7
Excess Air @ Sampling Point - %	24.1	19.9	20.6
Stack Temperature - °F	149	148	149
Stack Pressure – "Hg	29.64	29.92	29.90
Percent Isokinetic	98.8	96.6	95.9
Volume Dry Gas Sampled – DSCF*	30.843	30.956	30.261
Coke Burned – mlb	61.870	61.222	60.881
Particulates			
<u>Probe, Cyclone & Filter Catch</u> grains/dscf*	0.0525	0.0436	0.0190
grains/cf @ Stack Conditions	0.0341	0.0290	0.0125
lbs/hr	106.19	90.41	38.78
lb/mlb coke burned	1.72	1.48	0.64

* 29.92 "Hg, 68°F (760 mm Hg, 20°C)



DISCUSSION OF RESULTS

Duplicate sampling trains were performed for each of the three runs for a total of six tests.

The six tests for non-sulfuric acid particulate matter appeared to be valid representations of the actual emissions during the tests. All leak checks performed on the sampling train and the pitot tubes showed no leaks before or after each test. The indicative parameters calculated from the field data were in close agreement. The moisture percentages for the tests were within 7.4 percent of the mean value. The measured flow rates (Q_s) for the tests were within 3.6 percent of the mean value. The rates of sampling for the tests were within the specified limits (90 to 110 percent isokinetic). The greatest deviation from 100 percent isokinetic was 4.1 percent.

The calculated emissions (pounds per hour) of particulate matter for the six tests showed a range of -46.5 percent to +46.5 percent variation from the mean value.



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DESCRIPTION OF PROCESS

The FCC Flue Gas system takes Regenerator Flue Gas and reduces the CO, NO_x, SO_x, and catalyst fines so that the Flue Gas that is discharged meets the federally mandated standards. The Wet Gas Scrubber consists of a circulating caustic solution to remove SO₂ and catalyst fines, a Wet Electrostatic Precipitator to further remove residual catalyst fines and SO₃, and a stack to achieve a required discharge height and for continuous emission monitoring.



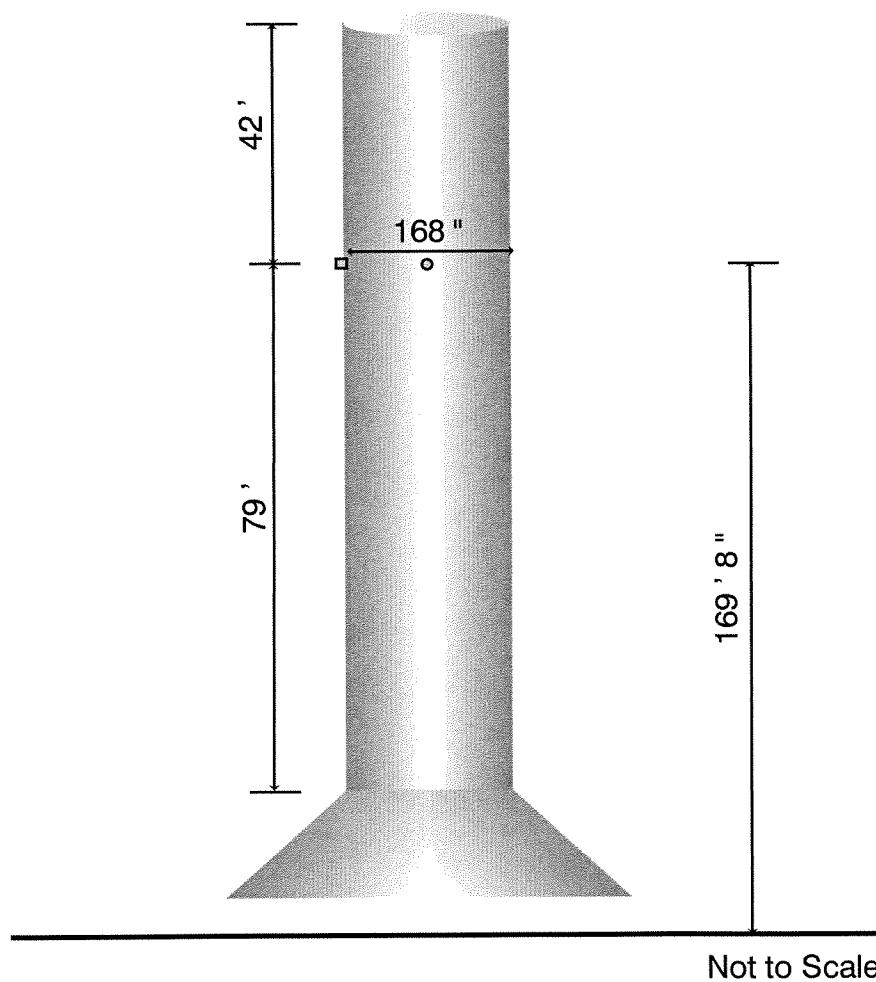
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DESCRIPTION OF SAMPLING LOCATION

The sampling location on the FCCU WESP Stack is 169 feet 8 inches above the ground. The sampling ports are located 79 feet (5.64 stack diameters) downstream from a constriction in the stack and 42 feet (3.00 stack diameters) upstream from the outlet of the stack.

SAMPLING LOCATION

FCCU WESP Stack



Not to Scale



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SAMPLING AND ANALYTICAL PROCEDURES

The sampling followed the procedures set forth in the Code of Federal Regulations, Title 40, Chapter I, Part 60, Appendix A, Methods 1, 2, 3B, 4, and 5B.

A preliminary velocity traverse was made at each of the four ports on the stack, in order to determine the uniformity and magnitude of the flow prior to testing. All traverse points were checked for cyclonic flow and the average angle of flow was equal to 2.5 degrees. Alternate procedures would be required if the angle of flow was greater than 20 degrees. Six traverse points were sampled from each of the four ports for a total of twenty-four traverse points.

The sampling trains were leak checked at the nozzle before each test, and again after each test at the highest vacuum reading recorded during the test. This was done to predetermine the possibility of a diluted sample.

The pitot tube lines were checked for leaks before and after each test under both a vacuum and a pressure. The lines were also checked for clearance and the manometer was zeroed before each test.

An integrated orsat sample was collected and analyzed according to EPA Method 3B during each test.

Non-Sulfuric Acid Particulate Matter

Six samples for non-sulfuric acid particulate matter were collected. The samples were taken according to EPA Methods 1, 2, 3B, 4, and 5B. For each run, samples of two and one-half minute duration were taken isokinetically at each of the twelve traverse points for a total sampling time of 60 minutes. Reagent blanks were submitted.



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The " front-half " of the sampling train contained the following components:

Stainless Steel Nozzle
Heated Glass Probe @ 320°F ± 25°F
Heated Glass Fiber Filter and Glass Support @ 320°F ± 25°F

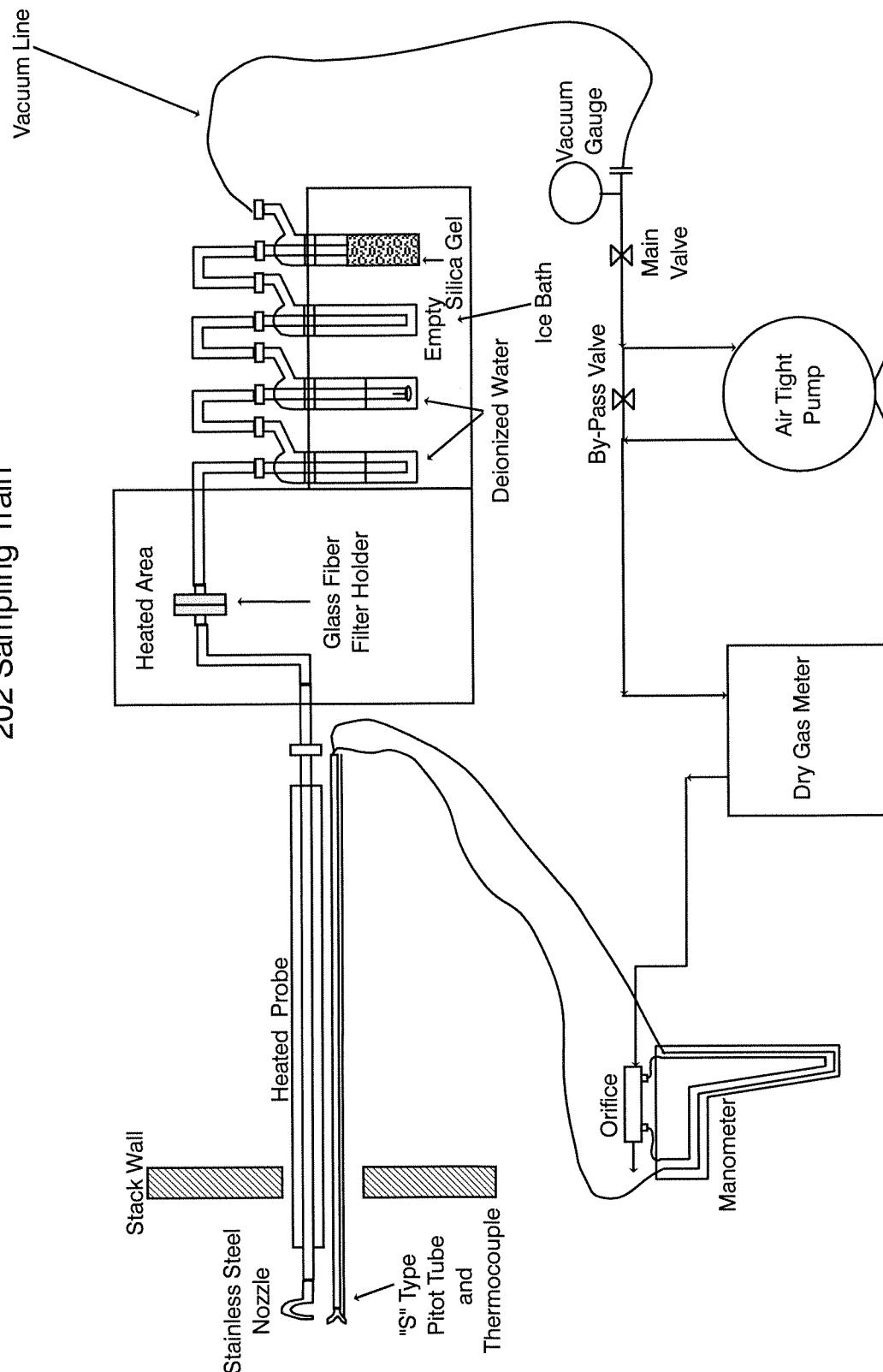
The " back-half " of the "A" sampling train contained the following components:

<u>Impinger Number</u>	<u>Contents</u>	<u>Amount</u>	<u>Parameter Collected</u>
1	Deionized Water	200 ml	Moisture
2	Deionized Water	200 ml	Moisture
3	Empty	-----	Moisture
4	Silica Gel	200 g	Moisture

The " back-half " of the "B" sampling train contained the following components:

Condenser Coil
Condensate Trap
Impinger 1 - Modified Design, Empty
Teflon Fiber Filter and Teflon Support @ ≤ 85°F
Impinger 3 - Modified Design, 100 ml Deionized Water
Impinger 4 - Modified Design, Silica Gel

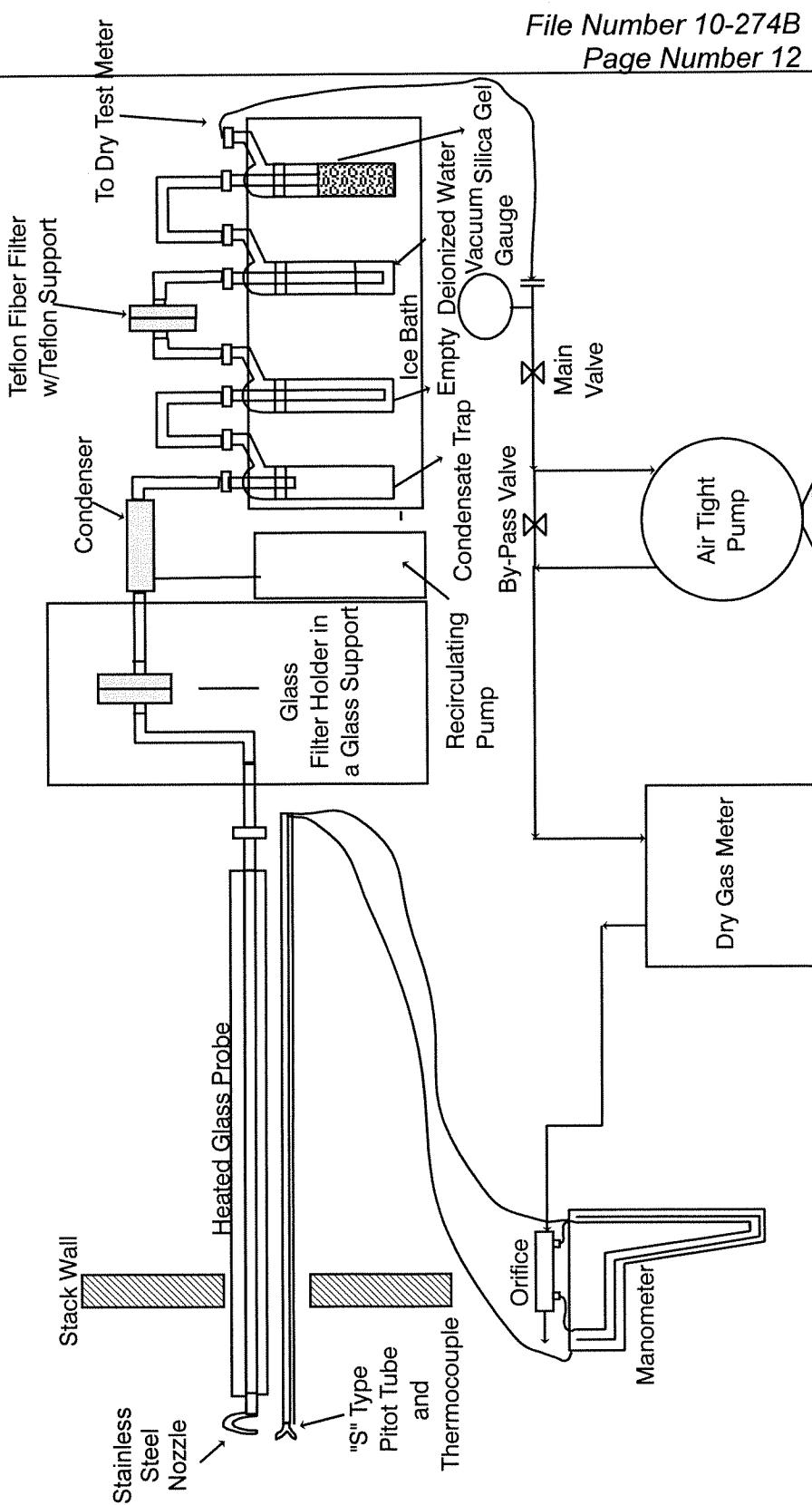
Particulate matter emissions were calculated from gravimetric analysis using only the "front-half " collections of the sampling train.

Schematic Diagram of the EPA Combined Method 5B/
202 Sampling Train



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Schematic Diagram of the EPA Combined Methods
5B and OTM-28 Sampling Train





DESCRIPTION OF TESTS

Personnel from METCO Environmental arrived at the plant at 6:30 p.m. on Tuesday, June 29, 2010. After meeting with plant personnel and attending a brief safety orientation, the equipment was moved onto the FCCU WESP Stack. The equipment was secured and all work was completed at 9:15 p.m.

On Wednesday, June 30, work began at 7:00 a.m. The preliminary data was collected. The first set of tests for non-sulfuric acid particulate matter began at 7:08 p.m. and was completed at 8:34 p.m. The samples were recovered. The equipment was secured for the night and all work was completed at 9:00 p.m.

On Thursday, July 1, work began at 8:00 a.m. The preliminary data was collected. The second set of tests for non-sulfuric acid particulate matter began at 12:08 p.m. Testing continued until completion of the third set of tests at 4:36 p.m.

The samples were recovered and the equipment was moved off of the stack and loaded into the sampling van. The samples were recovered and transported to METCO Environmental's laboratory in Dallas, Texas, for analysis and evaluation.

Field operations at CITGO Petroleum Corp., FCCU WESP Stack, located in Lemont, Illinois, were completed at 6:00 p.m. on Thursday, July 1, 2010.



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APPENDICES

- A. Location of Sampling Points
- B. Source Emissions Calculations
- C. Calibration Data
- D. Field Testing Data
- E. Analytical Data
- F. Plant Operational Data
- G. Chain of Custody
- H. Resumes of Test Personnel



APPENDIX A

Location of Sampling Points FCCU WESP Stack

The sampling ports are located 79 feet (5.64 stack diameters) downstream from a constriction in the stack and 42 feet (3.00 stack diameters) upstream from the outlet of the stack. The locations of the sampling points were calculated as follows:

Port and Wall Thickness = 13 3/4 inches

Inside Stack Diameter = 168 inches

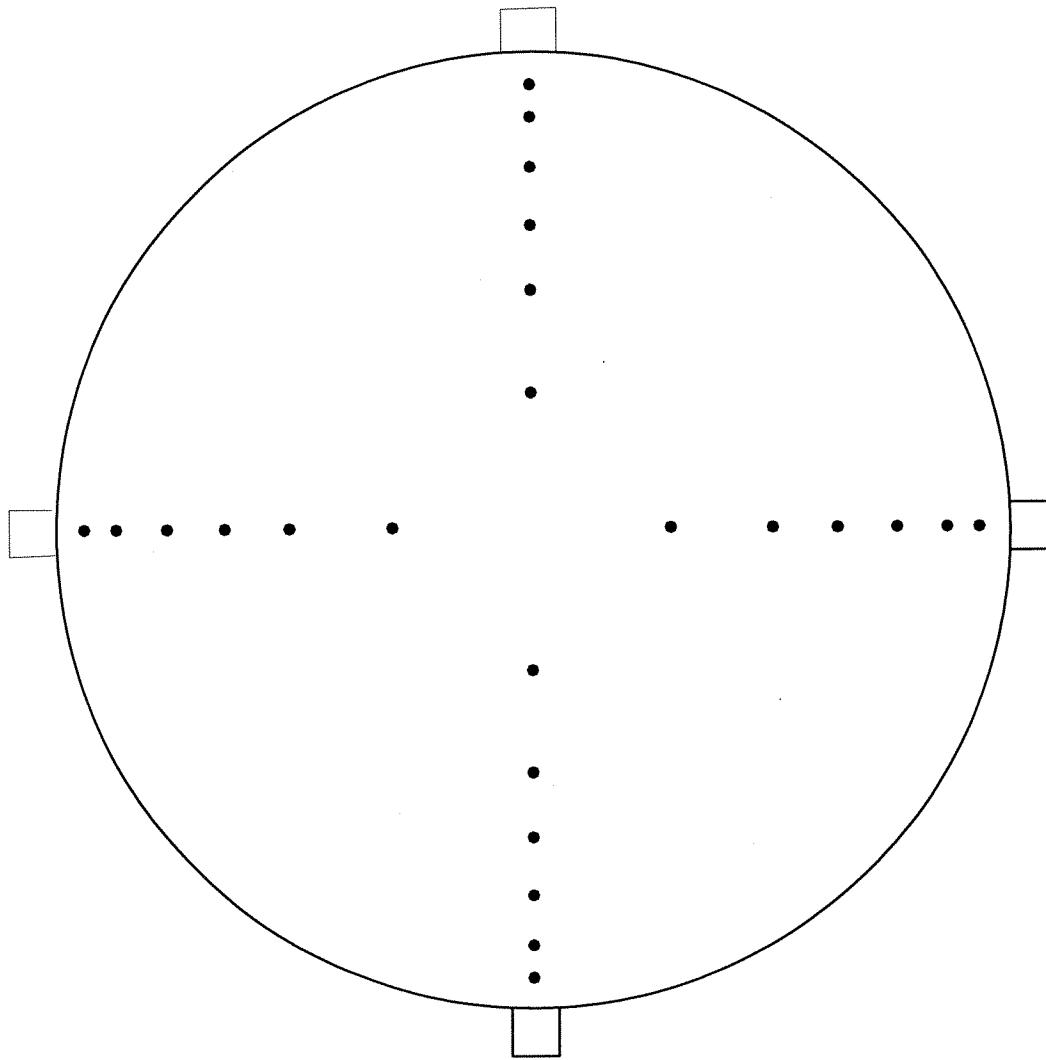
<u>Point Number*</u>	<u>Percent of Diameter From Wall</u>	<u>Distance From Wall</u>
1	2.1	3 1/2 "
2	6.7	11 1/4 "
3	11.8	19 13/16 "
4	17.7	29 3/4 "
5	25.0	42 "
6	35.6	59 13/16 "

* Calculated as one-half of a twelve point traverse

APPENDIX A

Location of Sampling Points

FCCU WESP Stack





APPENDIX B

Nomenclature and Equations for Calculation of Source Emissions



NOMENCLATURE FOR PARTICULATE CALCULATIONS

<u>Symbol</u>	<u>English</u>	<u>Metric</u>	<u>Description</u>
<u>Units</u>	<u>in.²</u>	<u>m²</u>	
A _s			Stack Area
C _{an}	gr/dscf*	g/dscm*	Particulate - probe, cyclone, and filter
C _{ao}	gr/dscf*	g/dscm*	Particulate - total
C _{at}	gr/CF @ stack conditions	g/m ³	Particulate - probe, cyclone, and filter
C _{au}	gr/CF @ stack conditions	g/m ³	Particulate - total
C _{aw}	lbs/hr	kg/hr	Particulate - probe, cyclone, and filter
C _{ax}	lbs/hr	kg/hr	Particulate - total
C _p			Pitot Tube Calibration Factor
D _n	in.	m	Sampling Nozzle Diameter
%EA			Percent Excess Air at sampling point
g	32.174 ft/sec ²		Acceleration of Gravity
%I			Percent Isokinetic
%M			Percent Moisture in the stack gas by volume
M _d			Mole fraction of dry gas



<u>Symbol</u>	<u>English Units</u>	<u>Metric Units</u>	<u>Description</u>
m_f	mg	mg	Particulate - probe, cyclone, and filter
M_{water}	18 lb/lb-mole		Molecular Weight of water
m_t	mg	mg	Particulate - total
MW	lb/lb-mole	g/g-mole	Molecular Weight of stack gas
MW_{air}	28.96 lb/lb-mole		Molecular Weight of air
MW_d	lb/lb-mole	g/g-mole	Molecular Weight of dry stack gas
P_b	"Hg Absolute	mm Hg	Barometric Pressure
P_m	"H ₂ O	mm H ₂ O	Orifice Pressure drop
P_s	"Hg Absolute	mm Hg	Stack Pressure
ΔP	"H ₂ O	mm H ₂ O	Velocity Head of stack gas
P_{std}	29.92 "Hg	760 mm Hg	Standard Barometric Pressure
Q_a	ACFM	m ³ /hr	Stack Gas Volume at actual stack conditions
Q_s	DSCFM*	dscm/hr*	Stack Gas Volume at 29.92 "Hg, 528°R, dry
R	21.83 "Hg-ft ³ /lb-mole°R		Universal Gas Constant
T_m	°F	°C	Average Gas Meter Temperature

* 29.92 " Hg, 68° F (760 mm Hg, 20° C)



<u>Symbol</u>	<u>English</u> <u>Units</u>	<u>Metric</u> <u>Units</u>	<u>Description</u>
	min	min	
T _t			Net time of test
T _s	°F	°C	Stack Temperature
T _{std}	528°R	293°K	Standard Temperature
V _m	ft ³	m ³	Volume of dry gas sampled @ meter conditions
V _{m_{std}}	dscf*	dscm*	Volume of dry gas sampled @ standard conditions
V _s	fpm	m/sec	Stack velocity @ stack conditions
V _w	ml	ml	Total water collected in impingers and silica gel
V _{w_{gas}}	scf*	scm*	Volume of water vapor collected @ standard conditions
ρ _{air}	0.0752 lbs/ft ³		Density of Air
ρ _{water}	1 g/ml		Density of Water
ρ _{man}	62.32 lbs/ft ³		Density of Manometer Oil

Standard Conditions: 29.92 "Hg, 68°F (760 mm Hg, 20°C)



EXAMPLE CALCULATIONS

1. Volume of dry gas sampled at standard conditions. *

$$Vm_{std} = Vm \left(\frac{T_{std}}{T_m + 460} \right) \left[\frac{P_b + \frac{P_m}{13.6}}{P_{std}} \right]$$

$$Vm_{std} = 17.65 Vm \left[\frac{P_b + \frac{P_m}{13.6}}{T_m + 460} \right] = dscf$$

$$Vm_{std} = dscf \times 0.028317 = dscm$$

2. Volume of water vapor collected at standard conditions. *

$$VW_{gas} = \frac{(V_w - gms\ SO_2 - gms\ H_2S) \rho_{water} R T_{std}}{P_{std} M_{water} 453.6}$$

$$VW_{gas} = 0.0472 (V_w - gms\ SO_2 - gms\ H_2S) = scf$$

$$VW_{gas} = scf \times 0.028317 = scm$$

3. Percent moisture in stack gas.

$$\%M = \frac{VW_{gas}}{Vm_{std} + VW_{gas}} \times 100 = \%$$



4. Mole fraction of dry gas.

$$M_d = \frac{100 - \%M}{100}$$

5. Average molecular weight of dry stack gas.

$$MW_d = \left[\%CO_2 \times \frac{44}{100} \right] + \left[\%O_2 \times \frac{32}{100} \right] + \left[\%N_2 \times \frac{28}{100} \right] + \left[\%CO \times \frac{28}{100} \right] = lb/lb - mole$$

$$= g/g - mole$$

6. Molecular weight of stack gas.

$$MW = MW_d \times M_d + 18(1 - M_d) = \frac{lb}{lb - mole} = g/g - mole$$

7. Percent excess air at sampling point.

$$\%EA = \frac{100 [\%O_2 - (0.5 \%CO)]}{0.265 (\%N_2) - [\%O_2 - (0.5 \%CO)]}$$

8. Stack Pressure.

$$P_s = P_b + \frac{\text{Stack Pressure } "H_2O}{13.6} = "Hg Absolute$$

$$P_s = "Hg Abs. \times 25.4 = mm Hg$$



9. Stack velocity at stack conditions.

$$V_s = C_p 60 \left[\frac{2g \times \rho_{man} \times P_{std} \times MW_{air} \times (T_s + 460)}{12 \times \rho_{air} \times P_s \times MW \times T_{std}} \right]^{1/2} \times \sqrt{\Delta P} \text{ average}$$

$$V_s = 5,123.8 C_p \left[\frac{(T_s + 460)}{P_s \times MW} \right]^{1/2} \sqrt{\Delta P} \text{ average} = fpm$$

$$V_s = fpm \times 0.00508 = m/sec$$

10. Dry stack gas volume at standard conditions. *

$$Q_s = \frac{1}{144} V_s \times A_s \times M_d \times \frac{T_{std}}{T_s + 460} \times \frac{P_s}{P_{std}}$$

$$Q_s = \frac{0.123 V_s \times A_s \times M_d \times P_s}{T_s + 460} = DSCFM$$

$$Q_s = DSCFM \times 1.6990 = dscm/hr$$

11. Actual stack gas volume at stack conditions.

$$Q_a = \frac{V_s \times A_s}{144} = ACFM$$

$$Q_a = ACFM \times 1.6990 = m^3/hr$$

* 29.92 " Hg, 68° F (760 mm Hg, 20° C) B-7



12. Percent Isokinetic.

$$\%I = \frac{Vm_{std} \times (T_s + 460) \times P_{std} \times 100 \times 144 \text{ in}^2/\text{ft}^2}{M_d \times T_{std} \times P_s \times T_t \times V_s \left(\frac{\pi \times D_n^2}{4} \right)}$$

$$\%I = \frac{1039 \times Vm_{std} \times (T_s + 460)}{M_d \times P_s \times T_t \times V_s \times D_n^2}$$

13. Particulate – probe, cyclone, and filter.

$$C_{an} = \frac{m_f}{Vm_{std}} \times \frac{1 \text{ gr}}{64.8 \text{ mg}}$$

$$C_{an} = 0.0154 \times \frac{m_f}{Vm_{std}} = \text{gr/dscf} *$$

$$C_{an} = \text{gr/dscf} \times 2.290 = \text{g/dscm} *$$

14. Particulate total.

$$C_{ao} = 0.0154 \times \frac{m_t}{Vm_{std}} = \text{gr/dscf} *$$

$$C_{ao} = \text{gr/dscf} \times 2.290 = \text{g/dscm} *$$



15. Particulate – probe, cyclone, and filter at stack conditions.

$$C_{at} = C_{an} \times \frac{P_s}{P_{std}} \times \frac{(T_{std})}{(T_s + 460)} \times M_d$$

$$C_{at} = \frac{17.65 \times C_{an} \times P_s \times M_d}{T_s + 460} = \text{gr/CF}$$

$$C_{at} = \text{gr/CF} \times 2.290 = \text{g/m}^3$$

16. Particulate – total, at stack conditions.

$$C_{au} = \frac{17.65 \times C_{ao} \times P_s \times M_d}{T_s + 460} = \text{gr/CF}$$

$$C_{au} = \text{gr/CF} \times 2.290 = \text{g/m}^3$$



17. Particulate – probe, cyclone, and filter.

$$C_{aw} = C_{an} \times Q_s \times \frac{60 \text{ min}}{1 \text{ hr}} \times \frac{1 \text{ lb}}{7000 \text{ gr}}$$

$$C_{aw} = 0.00857 \times C_{an} \times Q_s = \text{lbs/hr}$$

$$C_{aw} = \text{lbs/hr} \times 0.4536 = \text{kg/hr}$$

18. Particulate – total.

$$C_{ax} = 0.00857 \times C_{ao} \times Q_s = \text{lbs/hr}$$

$$C_{ax} = \text{lbs/hr} \times 0.4536 = \text{kg/hr}$$



SOURCE EMISSION SURVEY

JOB NUMBER: 10-274
 JOB NAME: CITGO
 LOCATION: LEMONT, IL
 UNIT TESTED: FCCU WESP STACK (5B/202)

SOURCE EMISSION CALCULATIONS

SYMBOL	DESCRIPTION	UNITS	RUN NUMBER		
			1	2	3
DATE			06/30/10	07/01/10	07/01/10
BEGIN TIME			1908	1208	1500
END TIME			2034	1346	1636
P(b)	BAROMETRIC PRESSURE	"Hg Abs. (mm Hg)	29.66 (753.00)	29.94 (760.00)	29.92 (760.00)
P(m)	ORIFICE PRESSURE DROP	"H ₂ O (mm H ₂ O)	0.980 (24.900)	0.982 (24.900)	0.979 (24.900)
	DGM CALIBRATION FACTOR		1.012	1.012	1.012
V(m)	VOLUME DRY GAS SAMPLED @ METER CONDITIONS	ft.^3 (m^3)	35.344 (1.001)	33.751 (0.956)	33.542 (0.950)
	LEAK CHECK VOLUME	ft.^3	0.000	0.000	0.000
T(m)	AVERAGE GAS METER TEMPERATURE	DEG.F (DEG.C)	81 (27)	85 (29)	89 (32)
V(m[std])*	VOLUME DRY GAS SAMPLED @ STANDARD CONDITIONS*	DSCF (DSCM)	34.284 (0.971)	32.804 (0.929)	32.342 (0.916)
V(w)	TOTAL WATER COLLECTED, IMPPINGERS & SILICA GEL	ml	201.4	216.3	211.3
V(w[gas])	VOLUME WATER VAPOR COLLECTED @ STANDARD CONDITIONS*	SCF (SCM)	9.506 (0.269)	10.209 (0.289)	9.973 (0.282)
%M	MOISTURE IN STACK GAS BY VOLUME	%	21.71	23.73	23.57
Md	MOL FRACTION OF DRY GAS		0.7829	0.7627	0.7643
Tt	NET TIME OF TEST	MINUTES	60	60	60

* 68 Deg.F, 29.92 "Hg (20 Deg.C, 760 mm Hg)



SOURCE EMISSION CALCULATIONS

JOB NUMBER: 10-274
 JOB NAME: CITGO
 LOCATION: LEMONT, IL
 UNIT TESTED: FCCU WESP STACK (5B/202)

SYMBOL	DESCRIPTION	UNITS	RUN NUMBER		
			1	2	3
CO2		%	14.3	14.4	14.5
O2		%	4.2	3.6	3.7
CO		%	0.0	0.0	0.0
N2		%	81.5	82.0	81.8
%EA	EXCESS AIR @ SAMPLING POINT	%	24.1	19.9	20.6
MWd	MOLECULAR WEIGHT OF DRY STACK GAS	LB/LB-MOLE (g/g-MOLE)	30.46 (30.46)	30.45 (30.45)	30.47 (30.47)
MW	MOLECULAR WEIGHT OF STACK GAS	LB/LB-MOLE (g/g-MOLE)	27.75 (27.75)	27.49 (27.49)	27.53 (27.53)
Cp	PITOT TUBE CALIBRATION		0.810	0.810	0.810
DELTA P	VELOCITY HEAD OF STACK GAS	"H2O (mm H2O)	0.466 (11.800)	0.466 (11.800)	0.466 (11.800)
DELTA P^(1/2)		"H2O	0.682	0.683	0.682
Ts	STACK TEMPERATURE	DEG. F (DEG. C)	148 (64)	147 (64)	147 (64)
Ps	STACK PRESSURE	"Hg Abs. (mm Hg) "H2O	29.64 (753.00) -0.32	29.92 (760.00) -0.32	29.90 (759.00) -0.34
Vs	STACK VELOCITY @ STACK CONDITIONS	FPM (m/SEC.)	2,434 (12)	2,435 (12)	2,431 (12)
As	STACK AREA	(SQ.INCHES) (SQ.METERS)	22,167 (14)	22,167 (14)	22,167 (14)
Qs	DRY STACK GAS VOLUME @ STANDARD CONDITIONS* WET STACK GAS VOLUME @ STANDARD CONDITIONS*	DSCFM (DSCM/HR) WSCFH	253,287 (430,335) 19,411,445	249,596 (424,008) 19,635,169	249,542 (423,972) 19,589,847
Qa	ACTUAL STACK GAS VOLUME @ STACK CONDITIONS	ACFM (m^3/HR)	374,617 (636,474)	374,859 (636,885)	374,164 (635,705)
Dn	SAMPLING NOZZLE DIAM.	IN. (m)	0.250 (0.006)	0.250 (0.006)	0.250 (0.006)
%I	PERCENT ISOKINETIC	%	102.2	99.3	97.9

* 68 Deg.F, 29.92 "Hg (20 Deg.C, 760 mm Hg)



SOURCE EMISSION CALCULATIONS

JOB NUMBER: 10-274
 JOB NAME: CITGO
 LOCATION: LEMONT, IL
 UNIT TESTED: FCCU WESP STACK (5B/202)

SYMBOL	DESCRIPTION	UNITS	RUN NUMBER		
			1	2	3
Mf	FILT. PARTICULATE - PROBE, CYCLONE AND FILTER	mg	92.5	68.2	40.1
Mt	COND. PARTICULATE - TOTAL	mg	---	---	---
Can	FILT. PARTICULATE - PROBE, CYCLONE AND FILTER	gr/DSCF* (g/DSCM)	0.0415 (0.0951)	0.0320 (0.0733)	0.0191 (0.0437)
Cao	COND. PARTICULATE - TOTAL	gr/DSCF* (g/DSCM)	---	---	---
Cat	FILT. PARTIC.-PROBE, CYCLONE AND FILTER @ STACK COND.	gr/CF (g/m ³)	0.0280 (0.0641)	0.0212 (0.0485)	0.0127 (0.0291)
Cau	COND. PARTICULATE - TOTAL @ STACK CONDITIONS	gr/CF (g/m ³)	---	---	---
Caw	FILT. PARTICULATE - PROBE, CYCLONE AND FILTER	LBS/HR (Kg/HR)	90.19 (40.91)	68.48 (31.06)	40.83 (18.52)
Cax	COND. PARTICULATE - TOTAL	LBS/HR (Kg/HR)	---	---	---

* 68 Deg.F, 29.92 "Hg (20 Deg.C, 760 mm Hg)



SOURCE EMISSION SURVEY

JOB NUMBER: 10-274
 JOB NAME: CITGO
 LOCATION: LEMONT, IL
 UNIT TESTED: FCCU WESP STACK (5B/OTM 28)

SOURCE EMISSION CALCULATIONS

SYMBOL	DESCRIPTION	UNITS	RUN NUMBER		
			1	2	3
DATE			06/30/10	07/01/10	07/01/10
BEGIN TIME			1908	1208	1500
END TIME			2034	1346	1636
P(b)	BAROMETRIC PRESSURE	"Hg Abs. (mm Hg)	29.66 (753.00)	29.94 (760.00)	29.92 (760.00)
P(m)	ORIFICE PRESSURE DROP	"H ₂ O (mm H ₂ O)	0.881 (22.400)	0.905 (23.000)	0.892 (22.700)
	DGM CALIBRATION FACTOR		1.000	1.000	1.000
V(m)	VOLUME DRY GAS SAMPLED @ METER CONDITIONS	ft.^3 (m^3)	31.863 (0.902)	31.914 (0.904)	31.276 (0.886)
	LEAK CHECK VOLUME	ft.^3	0.000	0.000	0.000
T(m)	AVERAGE GAS METER TEMPERATURE	DEG.F (DEG.C)	82 (28)	86 (30)	87 (31)
V(m[std])*	VOLUME DRY GAS SAMPLED @ STANDARD CONDITIONS*	DSCF (DSCM)	30.843 (0.873)	30.956 (0.877)	30.261 (0.857)
V(w)	TOTAL WATER COLLECTED, IMPINGERS & SILICA GEL	ml	210.0	200.9	201.2
V(w[gas])	VOLUME WATER VAPOR COLLECTED @ STANDARD CONDITIONS*	SCF (SCM)	9.912 (0.281)	9.482 (0.269)	9.497 (0.269)
%M	MOISTURE IN STACK GAS BY VOLUME	%	24.32	23.45	23.89
Md	MOL FRACTION OF DRY GAS		0.7568	0.7655	0.7611
Tt	NET TIME OF TEST	MINUTES	60	60	60

* 68 Deg.F, 29.92 "Hg (20 Deg.C, 760 mm Hg)



SOURCE EMISSION CALCULATIONS

JOB NUMBER: 10-274

JOB NAME: CITGO

LOCATION: LEMONT, IL

UNIT TESTED: FCCU WESP STACK (5B/OTM 28)

SYMBOL	DESCRIPTION	UNITS	RUN NUMBER		
			1	2	3
CO2		%	14.3	14.4	14.5
O2		%	4.2	3.6	3.7
CO		%	0.0	0.0	0.0
N2		%	81.5	82.0	81.8
%EA	EXCESS AIR @ SAMPLING POINT	%	24.1	19.9	20.6
MWd	MOLECULAR WEIGHT OF DRY STACK GAS	LB/LB-MOLE (g/g-MOLE)	30.46 (30.46)	30.45 (30.45)	30.47 (30.47)
MW	MOLECULAR WEIGHT OF STACK GAS	LB/LB-MOLE (g/g-MOLE)	27.43 (27.43)	27.53 (27.53)	27.49 (27.49)
Cp	PITOT TUBE CALIBRATION		0.820	0.820	0.820
DELTA P	VELOCITY HEAD OF STACK GAS	"H2O (mm H2O)	0.420 (10.700)	0.431 (10.900)	0.423 (10.700)
DELTA P^(1/2)		"H2O	0.646	0.653	0.647
Ts	STACK TEMPERATURE	DEG. F (DEG. C)	149 (65)	148 (64)	149 (65)
Ps	STACK PRESSURE	"Hg Abs. (mm Hg) "H2O	29.64 (753.00) -0.32	29.92 (760.00) -0.32	29.90 (759.00) -0.34
Vs	STACK VELOCITY @ STACK CONDITIONS	FPM (m/SEC.)	2,349 (12)	2,357 (12)	2,340 (12)
As	STACK AREA	(SQ.INCHES) (SQ.METERS)	22,167 (14)	22,167 (14)	22,167 (14)
Qs	DRY STACK GAS VOLUME @ STANDARD CONDITIONS* WET STACK GAS VOLUME @ STANDARD CONDITIONS*	DSCFM (DSCM/HR) WSCFH	235,905 (400,803) 18,702,828	242,089 (411,309) 18,974,971	238,409 (405,057) 18,794,561
Qa	ACTUAL STACK GAS VOLUME @ STACK CONDITIONS	ACFM (m^3/HR)	361,609 (614,374)	362,854 (616,489)	360,197 (611,975)
Dn	SAMPLING NOZZLE DIAM.	IN. (m)	0.250 (0.006)	0.250 (0.006)	0.250 (0.006)
%I	PERCENT ISOKINETIC	%	98.8	96.6	95.9

* 68 Deg.F, 29.92 "Hg (20 Deg.C, 760 mm Hg)



SOURCE EMISSION CALCULATIONS

JOB NUMBER: 10-274
 JOB NAME: CITGO
 LOCATION: LEMONT, IL
 UNIT TESTED: FCCU WESP STACK (5B/OTM 28)

SYMBOL	DESCRIPTION	UNITS	RUN NUMBER		
			1	2	3
Mf	FILT. PARTICULATE - PROBE, CYCLONE AND FILTER	mg	105.2	87.6	37.3
Mt	COND. PARTICULATE - TOTAL	mg	---	---	---
Can	FILT. PARTICULATE - PROBE, CYCLONE AND FILTER	gr/DSCF* (g/DSCM)	0.0525 (0.1203)	0.0436 (0.0998)	0.0190 (0.0435)
Cao	COND. PARTICULATE - TOTAL	gr/DSCF* (g/DSCM)	---	---	---
Cat	FILT. PARTIC.-PROBE, CYCLONE AND FILTER @ STACK COND.	gr/CF (g/m ³)	0.0341 (0.0781)	0.0290 (0.0664)	0.0125 (0.0286)
Cau	COND. PARTICULATE - TOTAL @ STACK CONDITIONS	gr/CF (g/m ³)	---	---	---
Caw	FILT. PARTICULATE - PROBE, CYCLONE AND FILTER	LBS/HR (Kg/HR)	106.19 (48.17)	90.41 (41.01)	38.78 (17.59)
Cax	COND.PARTICULATE - TOTAL	LBS/HR (Kg/HR)	---	---	---

* 68 Deg.F, 29.92 "Hg (20 Deg.C, 760 mm Hg)



APPENDIX C

Calibration Data

<u>Equipment</u>	<u>Calibration Factor</u>	<u>Calibration Date</u>
Pitot Tube #T4-E-6	0.810	06/11/10
Pitot Tube #T4-E-8	0.820	07/07/10
Probe Tip #10-274-I	0.250	06/30/10
Probe Tip #10-274-II	0.250	06/30/10
Dry Gas Meter #49-5	1.012	05/25/10
Stack Unit Orifice #49-5		06/02/10
Digital Temperature Indicator #49-5		05/25/10
Dry Gas Meter #T2-4	1.000	04/19/10
Stack Unit Orifice # T2-4		01/05/10
Digital Temperature Indicator # T2-4		04/19/10
Barometer #49-2		05/24/10



Pitot Tube Calibration

Date: 6/11/10Time: 1600Pitot No: T4-E-6T_s: 74Pitot Dimensions: 12' x 3/8"C_{pstd}: 0.990

Pitot Inspections

Pitot tips level and perpendicular

YES / NO

Pitot tips free from obstruction

YES / NO

Pitot tips damaged

YES / NO

Motor Setting	fps mark	Calibration Standard		Standard Average	High	$\sqrt{\text{High}}$	Cal. Factor	Low	$\sqrt{\text{Low}}$	Cal. Factor
		Start	End							
7	20	0-10	0-10	0.316	0.15	0.387	0.808	0.15	0.387	0.808
14	30	0-20	0-20	0.447	0.30	0.548	0.808	0.29	0.539	0.822
20	40	0.36	0.36	0.600	0.54	0.735	0.808	0.53	0.728	0.816
28	50	0.56	0.56	0.748	0.85	0.922	0.804	0.82	0.906	0.818
35	60	0.80	0.80	0.894	1.20	1.095	0.808	1.20	1.095	0.808
41	70	1.10	1.10	1.049	1.60	1.265	0.821	1.60	1.265	0.821
50	80	1.40	1.40	1.183	2.10	1.449	0.808	2.00	1.414	0.828
62	90	1.80	1.80	1.342	2.65	1.628	0.816	2.55	1.597	0.832
28*	50*	0.56	0.56	0.748	0.85	0.922	0.804	0.82	0.906	0.818
28*	50*	0.56	0.56	0.748	0.85	0.922	0.804	0.82	0.906	0.818
Average								0.810		0.819

*not included in average

$$C_p = C_{pstd} \left(\frac{\sqrt{\Delta P_{std}}}{\sqrt{\Delta P}} \right)$$

Summary of Results:

Normal high side calibration factor 0.810variation + 1.36% variation - 0.74%Normal low side calibration factor 0.819variation + 1.59% variation - 1.34%Calibrator: FreemanOffice: DallasQA/QC Check
Completeness Legibility Accuracy Specifications Reasonableness Checked by: JCutler



Pitot Tube Calibration

Date: 7/7/2010Time: 1000Pitot No: T4E8T_s: 70Pitot Dimensions: 3/8C_{psdt}: 0.990

Pitot Inspections

Pitot tips level and perpendicular

YES / NO

Pitot tips free from obstruction

YES / NO

Pitot tips damaged

YES / NO

Motor Setting	fps mark	Calibration Standard		Standard Average	High	$\sqrt{\text{High}}$	Cal. Factor	Low	$\sqrt{\text{Low}}$	Cal. Factor
		Start	End							
7	20	0.10	0.10	0.316	0.15	0.387	0.808	0.15	0.387	0.808
14	30	0.20	0.20	0.447	0.29	0.539	0.821	0.29	0.539	0.821
20	40	0.36	0.36	0.600	0.52	0.714	0.824	0.52	0.721	0.824
28	50	0.56	0.56	0.748	0.81	0.900	0.823	0.81	0.900	0.823
35	60	0.80	0.80	0.894	1.20	1.095	0.808	1.20	1.095	0.808
41	70	1.10	1.10	1.049	1.60	1.265	0.821	1.60	1.265	0.821
50	80	1.40	1.40	1.183	2.00	1.414	0.828	2.00	1.414	0.828
62	90	1.80	1.80	1.342	2.60	1.612	0.824	2.60	1.581	0.824
28*	50*	0.56	0.56	0.748	0.81	0.900	0.823	0.81	0.900	0.823
28*	50*	0.56	0.56	0.748	0.81	0.900	0.823	0.81	0.900	0.823
Average										

*not included in average

$$C_p = C_{psdt} \left(\frac{\sqrt{\Delta P_{std}}}{\sqrt{\Delta P}} \right)$$

Summary of Results:

Normal high side calibration factor 0.820variation + 0.97 variation - 1.46Normal low side calibration factor 0.819variation + 1.10 variation - 1.34Calibrator: Michael SaporitoOffice: DallasQA/QC Check
Completeness Legibility Accuracy Specifications Reasonableness Checked by: Kyle Gilbert

Nozzle Calibration

Nozzle Set No. _____

Caliper ID: T-6 _____Date: 6/30/10 _____Calibrator: JC _____Office/Location: Dallas _____

1	2	3	4	5	6
Reading 1 <u>0.250</u>	<u>0.250</u>	_____	_____	_____	_____
Reading 2 <u>0.257</u>	<u>0.250</u>	_____	_____	_____	_____
Reading 3 <u>0.250</u>	<u>0.250</u>	_____	_____	_____	_____
Reading 4 <u>0.250</u>	<u>0.249</u>	_____	_____	_____	_____
Reading 5 <u>0.250</u>	<u>0.250</u>	_____	_____	_____	_____
Reading 6 <u>0.250</u>	<u>0.250</u>	_____	_____	_____	_____
Reading 7 <u>0.250</u>	<u>0.250</u>	_____	_____	_____	_____
Reading 8 <u>0.250</u>	<u>0.250</u>	_____	_____	_____	_____
Reading 9 <u>0.250</u>	<u>0.250</u>	_____	_____	_____	_____
Reading 10 <u>0.250</u>	<u>0.250</u>	_____	_____	_____	_____
<u>10-274-I</u>		<u>10-274-II</u>			
Average <u>0.250</u>	<u>0.250</u>	_____	_____	_____	_____
7	8	9	10	11	12
Reading 1 _____	_____	_____	_____	_____	_____
Reading 2 _____	_____	_____	_____	_____	_____
Reading 3 _____	_____	_____	_____	_____	_____
Reading 4 _____	_____	_____	_____	_____	_____
Reading 5 _____	_____	_____	_____	_____	_____
Reading 6 _____	_____	_____	_____	_____	_____
Reading 7 _____	_____	_____	_____	_____	_____
Reading 8 _____	_____	_____	_____	_____	_____
Reading 9 _____	_____	_____	_____	_____	_____
Reading 10 _____	_____	_____	_____	_____	_____
Average _____	_____	_____	_____	_____	_____

 QA/QC Check
 Completeness Legibility Accuracy Specifications Reasonableness
Checked by: C-4 C-4

10-274B

Dry Gas Meter CalibrationDry Gas Meter Number 49-5Date: 5-25-14 ΔH
(°H₂O)C_{dg}

0.50

1.017 ✓

1.00

1.015 ✓

1.50

1.013 ✓

2.00

1.012 ✓

3.00

1.007 ✓

4.00

1.007 ✓

Average

1.012 ✓Variation: + 0.50%
- 0.49%Adjustment Required: Yes No XCalibrator: Office: Clancy Hill, NJQA/QC Check
Completeness Legibility Accuracy Specifications Reasonableness Checked by: R. Bell



DRY GAS METER CALIBRATION

Meter Number: 49-5Date: 5-25-10Wet Test Meter No: 8Calibrator: R. J. Jones

$$\text{Wet Test Meter } VM_{\text{std}} = 17.65 \times V_m \quad \frac{P_b + \frac{P_m}{13.6}}{T_m + 460} \times C_f = \text{scf}$$

$$\text{Dry Test Meter } VM_{\text{std}} = 17.65 \times V_m \quad \frac{P_b + \frac{P_m}{13.6}}{T_m + 460} = \text{scf}$$

Run No: 100.5 ✓ "H₂OP_b: 30.20 "HgWet Test Meter C_f: 1.000Control Module Vacuum: 5 "HgWet Test MeterDry Gas Meter

Time	Meter Reading	T _m	P _m	Meter Reading	T _m	Inlet	Outlet	P _m
End	803 7.543	66 °F	-2.2 "H ₂ O	401.787	71 °F	67 °F		0.5 "H ₂ O
Start	747 0.000	66 °F	-2.2 "H ₂ O	394.389	70 °F	65 °F		0.5 "H ₂ O
	10 7.543 ✓ cf ^A	66 °F _{avg}	-2.2 "H ₂ O _{avg}	7.318 ✓ cf ^A	68 °F _{avg}	69 °F _{avg}		0.5 "H ₂ O _{avg}

cf^A = V_m

$$\text{Wet Test Meter } VM_{\text{std}} = 17.65 \times \underline{7.543} \quad \frac{30.20 + \frac{-2.2}{13.6}}{66 + 460} \times \underline{1.000} C_f = \underline{7.603} \text{ scf}$$

$$\text{Dry Gas Meter } VM_{\text{std}} = 17.65 \times \underline{7.318} \quad \frac{30.20 + \frac{0.5}{13.6}}{68 + 460} = \underline{7.478} \text{ scf}$$

$$\text{Calibration Factor (C}_{dg}\text{)} = \frac{\text{Wet Test Meter } VM_{\text{std}}}{\text{Dry Gas Meter } VM_{\text{std}}} \quad C_{dg} = \frac{7.603}{7.478} = \underline{1.017} \checkmark$$

QA/QC Check

Completeness Legibility Accuracy Specifications Reasonableness Checked by: R. J. Jones



DRY GAS METER CALIBRATION

Meter Number: 49-S
 Date: 5-25-10

Wet Test Meter No: 8
 Calibrator: R. Jones

$$\text{Wet Test Meter } VM_{\text{std}} = 17.65 \times V_m \quad \frac{P_b + \frac{P_m}{13.6}}{T_m + 460} \times C_f = \text{ scf}$$

$$\text{Dry Test Meter } VM_{\text{std}} = 17.65 \times V_m \quad \frac{P_b + \frac{P_m}{13.6}}{T_m + 460} = \text{ scf}$$

Run No: 1@ 1.0 ✓ "H₂O
 Wet Test Meter C_f: 1.000

P_b: 30.20 "Hg
 Control Module Vacuum: 5 "Hg

Wet Test MeterDry Gas Meter

	Time	Meter Reading	T _m	P _m	Meter Reading	Inlet T _m	Outlet T _m	P _m
End	<u>8:16</u>	<u>7.053</u>	<u>66°F</u>	<u>-32 "H₂O</u>	<u>409.114</u>	<u>74 °F</u>	<u>68 °F</u>	<u>1.0 "H₂O</u>
Start	<u>8:05</u>	<u>0.000</u>	<u>66°F</u>	<u>-32 "H₂O</u>	<u>402.186</u>	<u>71 °F</u>	<u>67 °F</u>	<u>1.0 "H₂O</u>
c ^A = V _m		<u>11 7.053</u>	<u>c^A</u>	<u>66 °F_{avg}</u>	<u>-32 "H₂O_{avg}</u>	<u>6.928</u>	<u>c^A</u>	<u>1.0 "H₂O_{avg}</u>

$$\text{Wet Test Meter } VM_{\text{std}} = 17.65 \times \frac{7.053}{66 + 460} \times \frac{30.20 + \frac{-32}{13.6}}{70 + 460} \times 1.000 C_f = \frac{7.092}{6.985} \text{ scf}$$

$$\text{Dry Gas Meter } VM_{\text{std}} = 17.65 \times \frac{6.928}{70 + 460} \times \frac{30.20 + \frac{1.0}{13.6}}{70 + 460} = \frac{6.985}{6.985} \text{ scf}$$

$$\text{Calibration Factor (C}_{dg}\text{)} = \frac{\text{Wet Test Meter } VM_{\text{std}}}{\text{Dry Gas Meter } VM_{\text{std}}} \quad C_{dg} = \frac{7.092}{6.985} = \frac{1.015}{1.015}$$

QA/QC Check
 Completeness Legibility Accuracy Specifications Reasonableness

Checked by: RJ RE



DRY GAS METER CALIBRATION

Meter Number: 49-5Date: 5-25-07Wet Test Meter No: 8Calibrator: R Jones

$$\text{Wet Test Meter } VM_{std} = 17.65 \times V_m \quad \frac{P_b + \frac{P_m}{13.6}}{T_m + 460} \times C_f = \text{ scf}$$

$$\text{Dry Test Meter } VM_{std} = 17.65 \times V_m \quad \frac{P_b + \frac{P_m}{13.6}}{T_m + 460} = \text{ scf}$$

Run No: 1@1.5 "H₂OP_b: 30.20 "HgWet Test Meter C_f: 1.000Control Module Vacuum: 5 "HgWet Test Meter

	Meter	Time	Reading	T _m	P _m
End	832	10.511		66 °F	-4.2 "H ₂ O
Start	618	0.000		66 °F	-4.2 "H ₂ O
cf ^A = V _m		14	10.511 ✓	66 °F _{avg}	-4.2 "H ₂ O _{avg}

Dry Gas Meter

	Meter	T _m	Inlet	Outlet	P _m
End	498	76 °F	70 °F		1.5 "H ₂ O
Start	409.503	72 °F	68 °F		1.5 "H ₂ O
cf ^A = V _m		10.349 ✓	cf ^A	72 ✓ °F _{avg}	1.5 "H ₂ O _{avg}

$$\text{Wet Test Meter } VM_{std} = 17.65 \times \frac{10.511}{66} \frac{30.20 + \frac{-4.2}{13.6}}{+460} \times 1.000 C_f = \frac{10.543}{10.407} \text{ scf}$$

$$\text{Dry Gas Meter } VM_{std} = 17.65 \times \frac{10.349}{72} \frac{30.20 + \frac{1.5}{13.6}}{+460} = \frac{10.407}{10.407} \text{ scf}$$

$$\text{Calibration Factor (C}_{dg}\text{)} = \frac{\text{Wet Test Meter } VM_{std}}{\text{Dry Gas Meter } VM_{std}}$$

$$C_{dg} = \frac{10.543}{10.407} = \underline{1.013}$$

QA/QC Check

Completeness Legibility Accuracy Specifications Reasonableness Checked by: R. Bell



DRY GAS METER CALIBRATION

Meter Number: 49-5
 Date: 5-25-10

Wet Test Meter No: 8
 Calibrator: R. Jones

$$\text{Wet Test Meter } VM_{\text{std}} = 17.65 \times V_m \quad \frac{P_b + \frac{P_m}{13.6}}{T_m + 460} \times C_f = \text{ scf}$$

$$\text{Dry Test Meter } VM_{\text{std}} = 17.65 \times V_m \quad \frac{P_b + \frac{P_m}{13.6}}{T_m + 460} = \text{ scf}$$

Run No: 1020 "H₂O
 Wet Test Meter C_f: 1.012

P_b: 30.20 "Hg
 Control Module Vacuum: 5 "Hg

Wet Test Meter

Time	Meter Reading	T _m	P _m		Meter Reading	T _m	Inlet	Outlet	P _m
End	847 10.855	66 °F	-5.2 "H ₂ O		431.104	77 °F	71 °F	2.0 "H ₂ O	
Start	834 0.000	66 °F	-5.2 "H ₂ O		420.422	74 °F	70 °F	2.0 "H ₂ O	
	13 10.855 ✓ cf ^A	66 °F _{avg}	-5.2 "H ₂ O _{avg}		10.682 ✓ cf ^A	73 ✓ °F _{avg}		2.0 "H ₂ O _{avg}	

$$\text{cf}^A = V_m$$

$$\text{Wet Test Meter } VM_{\text{std}} = 17.65 \times \frac{10.855}{66} \quad \frac{30.20 + \frac{-5.2}{13.6}}{66 + 460} \times \frac{1.012}{10.682} C_f = \frac{10.861}{10.735} \text{ scf}$$

$$\text{Dry Gas Meter } VM_{\text{std}} = 17.65 \times \frac{10.682}{73} \quad \frac{30.20 + \frac{2.0}{13.6}}{73 + 460} = \frac{10.735}{10.735} \text{ scf}$$

$$\text{Calibration Factor (C}_{dg}\text{)} = \frac{\text{Wet Test Meter } VM_{\text{std}}}{\text{Dry Gas Meter } VM_{\text{std}}} \quad C_{dg} = \frac{10.861}{10.735} = \underline{1.012} \text{ ✓}$$

QA/QC Check
 Completeness Legibility Accuracy Specifications Reasonableness

Checked by: R. Jones



DRY GAS METER CALIBRATION

Meter Number: 49-5
 Date: 5-25-10

Wet Test Meter No: 8
 Calibrator: R Jones

$$\text{Wet Test Meter } VM_{\text{std}} = 17.65 \times V_m \quad \frac{P_b + \frac{P_m}{13.6}}{T_m + 460} \times C_f = \text{ scf}$$

$$\text{Dry Test Meter } VM_{\text{std}} = 17.65 \times V_m \quad \frac{P_b + \frac{P_m}{13.6}}{T_m + 460} = \text{ scf}$$

Run No: 1030 "H₂O
 Wet Test Meter C_f: 1.00

P_b: 30.20 "Hg
 Control Module Vacuum: 5 "Hg

Wet Test Meter

	Meter			
Time	Reading	T _m	P _m	
End	903 13910	67 °F	-6.9 "H ₂ O	445.268
Start	849 0.000	67 °F	-6.9 "H ₂ O	431.579
	14 13,910 cf ^A	67 °F _{avg}	-6.9 "H ₂ O _{avg}	13,689 cf ^A

Dry Gas Meter

	Meter				
Time	Reading	T _m	Inlet	Outlet	P _m
End	80	°F	72	°F	3.0 "H ₂ O
Start	76	°F	71	°F	3.0 "H ₂ O

$$\text{Wet Test Meter } VM_{\text{std}} = 17.65 \times \frac{13.910}{67} \times \frac{30.20 + \frac{-6.9}{13.6}}{+460} \times 1.000 C_f = \frac{13.833}{13.738} \text{ scf}$$

$$\text{Dry Gas Meter } VM_{\text{std}} = 17.65 \times \frac{13.689}{78} \times \frac{30.20 + \frac{3.0}{13.6}}{+460} = \frac{13.738}{13.738} \text{ scf}$$

$$\text{Calibration Factor (C}_{dg}\text{)} = \frac{\text{Wet Test Meter } VM_{\text{std}}}{\text{Dry Gas Meter } VM_{\text{std}}} \quad C_{dg} = \frac{13.833}{13.738} = \underline{1.007}$$

QA/QC Check
 Completeness Legibility Accuracy Specifications Reasonableness

Checked by: R sell



DRY GAS METER CALIBRATION

Meter Number: 49-5
 Date: 5-25-10

Wet Test Meter No: 8
 Calibrator: K Jones

$$\text{Wet Test Meter } VM_{std} = 17.65 \times V_m \quad \frac{P_b + \frac{P_m}{13.6}}{T_m + 460} \times C_f = \text{ scf}$$

$$\text{Dry Test Meter } VM_{std} = 17.65 \times V_m \quad \frac{P_b + \frac{P_m}{13.6}}{T_m + 460} = \text{ scf}$$

Run No: 10401 "H₂O
 Wet Test Meter C_f: 1.000

P_b: 30.20 "Hg
 Control Module Vacuum: 5 "Hg

Wet Test Meter

Time	Meter Reading	T _m	P _m
End	914 10.752	67 °F	-9.6 "H ₂ O
Start	905 0.000	67 °F	-9.6 "H ₂ O
cf ^A = V _m	9 10.752 cf ^A	67 °F _{avg}	-9.6 "H ₂ O _{avg}

Dry Gas Meter

Meter	Reading	T _m	Inlet	Outlet	P _m
End	456.684	82 °F	73 °F	4.0 "H ₂ O	
Start	446.159	79 °F	72 °F	4.0 "H ₂ O	
cf ^A = V _m	10.525 cf ^A	77 °F _{avg}	4.0 "H ₂ O _{avg}		

$$\text{Wet Test Meter } VM_{std} = 17.65 \times \frac{10.752}{67} \times \frac{30.20 + \frac{-9.6}{13.6}}{+460} \times \frac{1.000}{10.525} C_f = \frac{10.626}{10.525} \text{ scf}$$

$$\text{Dry Gas Meter } VM_{std} = 17.65 \times \frac{10.525}{77} \times \frac{30.20 + \frac{4.0}{13.6}}{+460} = \frac{10.549}{10.525} \text{ scf}$$

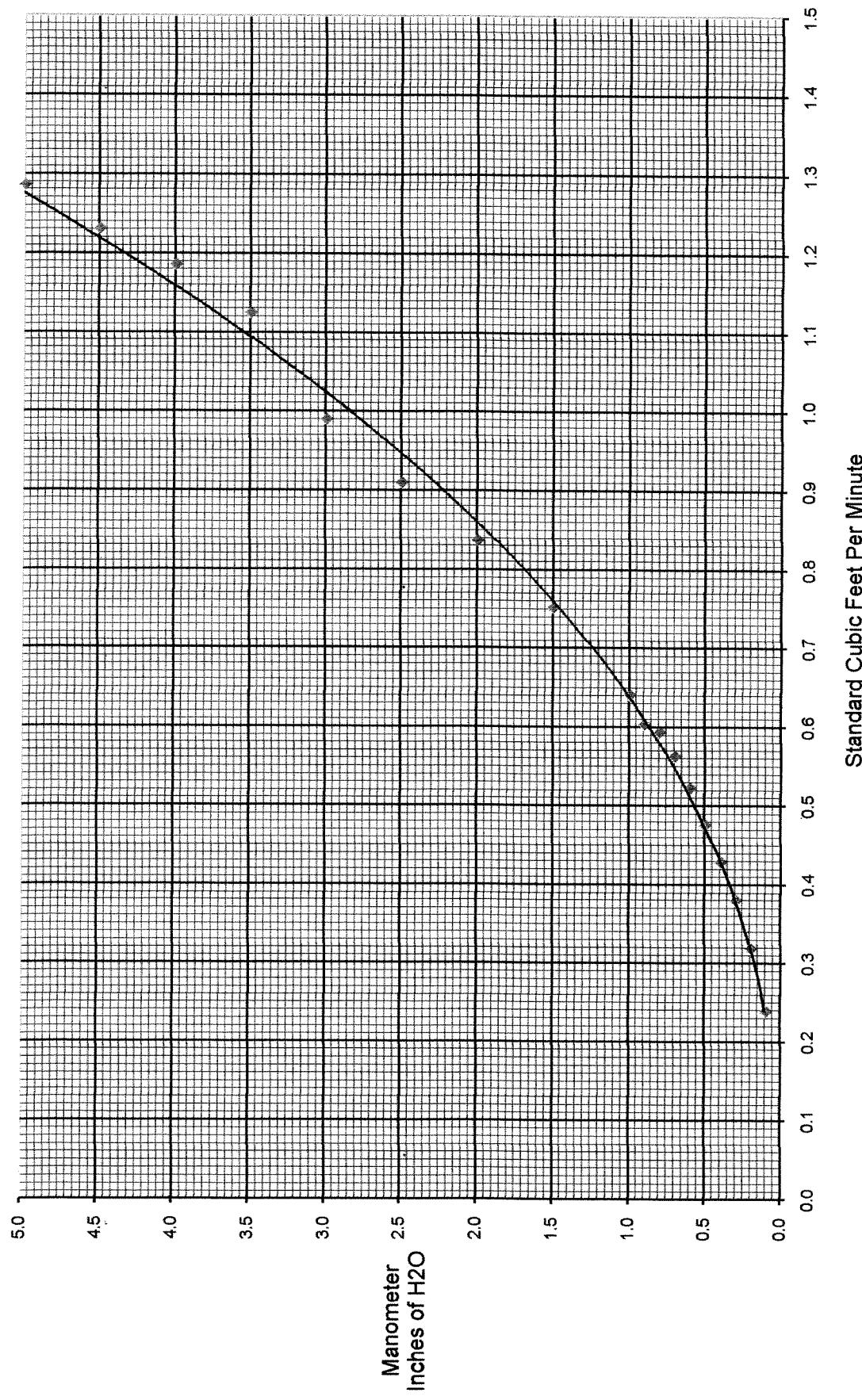
$$\text{Calibration Factor (C}_{dg}\text{)} = \frac{\text{Wet Test Meter } VM_{std}}{\text{Dry Gas Meter } VM_{std}} \quad C_{dg} = \frac{10.626}{10.549} = \frac{1.007}{1.007}$$

QA/QC Check
 Completeness Legibility Accuracy Specifications Reasonableness

Checked by: R. Schul

STACK UNIT ORIFICE NO: 49-5 DATE: 06/02/10 CALIBRATED BY: RYAN JONES

CHECKED BY: 0





Digital Temperature Indicator No. 49-5

Calibration Data

Date: 5-25-10

Reference Thermometer No. I - IV

Media	Time	Reference Thermometer (°F)	DTI (°F)
Ambient Air	<u>734</u>	<u>66</u>	<u>66 ✓</u>
Ice Bath	<u>737</u>	<u>33</u>	<u>33 ✓</u>
Boiling Water	<u>749</u>	<u>213</u>	<u>214 ✓</u>
Oven 250	<u>812</u>	<u>248</u>	<u>248 ✓</u>
Oven 300	<u>821</u>	<u>308</u>	<u>309 ✓</u>
Oven 350	<u>837</u>	<u>346</u>	<u>347 ✓</u>
Oven 375	<u>850</u>	<u>370</u>	<u>371 ✓</u>
Meter Adjusted?	YES	NO	X

Calibrator Lynn Jones

Office: Cherry Hill, NJ

QA/QC Check

Completeness Legibility Accuracy Specifications Reasonableness

Checked by: RE sell



Dry Gas Meter Calibration

Dry Gas Meter Number 72-4

Date: 4-19-10

ΔH
($^{\circ}\text{H}_2\text{O}$)

C_{dg}

0.50	<u>1.004 ✓</u>
1.00	<u>1.003 ✓</u>
1.50	<u>1.001 ✓</u>
2.00	<u>0.998 ✓</u>
3.00	<u>0.998 ✓</u>
4.00	<u>0.993 ✓</u>

Average 1.000 ✓

Variation: + 0.60 ✓ %
- 0.70 ✓ %

Adjustment Required: Yes No ✓

Calibrator: Ryan Will

Office: Houston

QA/QC Check

Completeness ✓ Legibility ✓ Accuracy ✓ Specifications ✓ Reasonableness ✓

Checked by: B. Ehl



DRY GAS METER CALIBRATION

Meter Number: TZ-4
 Date: 4-19-10

Wet Test Meter No: 2
 Calibrator: R. Williams

$$\text{Wet Test Meter } VM_{\text{std}} = 17.65 \times V_m \quad \frac{P_b + \frac{P_m}{13.6}}{T_m + 460} \times C_f = \text{scfm}$$

$$\text{Dry Test Meter } VM_{\text{std}} = 17.65 \times V_m \quad \frac{P_b + \frac{P_m}{13.6}}{T_m + 460} = \text{scfm}$$

Run No: 1 @ 0.50 ✓ "H₂O
 Wet Test Meter C_f: 0.998

P_b: 29.94 "Hg
 Control Module Vacuum: 5.0 "Hg

Wet Test Meter

Time	Meter Reading	T _m	P _m	Meter Reading	T _m	Inlet	Outlet	P _m
End 13:01	5.140	73 °F	-1.40 "H ₂ O	326.155		74	72 °F	0.50 "H ₂ O
Start 0:00	0.000	73 °F	-1.40 "H ₂ O	321.040		73	70 °F	0.50 "H ₂ O
	5.140 ✓ cf ^A	73 ✓ °F _{avg}	-1.40 "H ₂ O _{avg}	5.075 ✓ cf ^A	73 ✓ °F _{avg}	✓	0.50 "H ₂ O _{avg}	

cf^A = V_m

$$\text{Wet Test Meter } VM_{\text{std}} = 17.65 \times \frac{5.140}{73} \times \frac{29.94 + \frac{-1.40}{13.6}}{73 + 460} \times 0.998 C_f = \frac{5.069}{5.041} \text{ scfm}$$

$$\text{Dry Gas Meter } VM_{\text{std}} = 17.65 \times \frac{5.075}{73} \times \frac{29.94 + \frac{0.50}{13.6}}{73 + 460} = \frac{5.041}{5.041} \text{ scfm}$$

$$\text{Calibration Factor (C}_{dg}\text{)} = \frac{\text{Wet Test Meter } VM_{\text{std}}}{\text{Dry Gas Meter } VM_{\text{std}}} \quad C_{dg} = \frac{5.069}{5.041} = \underline{\underline{1.006}}$$

QA/QC Check
 Completeness Legibility Accuracy Specifications Reasonableness

Checked by: RB SL

10-274B



DRY GAS METER CALIBRATION

Meter Number: T2-4
 Date: 4-19-10

Wet Test Meter No: 2
 Calibrator: R.W.114-2

$$\text{Wet Test Meter } VM_{\text{std}} = 17.65 \times V_m \quad \frac{P_b + \frac{P_m}{13.6}}{T_m + 460} \times C_f = \text{scfm}$$

$$\text{Dry Test Meter } VM_{\text{std}} = 17.65 \times V_m \quad \frac{P_b + \frac{P_m}{13.6}}{T_m + 460} = \text{scfm}$$

Run No: 1@ 1.00 "H₂O
 Wet Test Meter C_f: 0.998

P_b: 29.94 "Hg
 Control Module Vacuum: 5.0 "Hg

Wet Test Meter

Time	Meter Reading	T _m	P _m	Meter Reading	Inlet T _m	Outlet T _m	P _m
End	5.160	73 °F	-2.00 "H ₂ O	331.580	77 °F	74 °F	1.00 "H ₂ O
Start	0.000	73 °F	-2.00 "H ₂ O	324.463	75 °F	73 °F	1.00 "H ₂ O
cf ^A = V _m	5.160 ✓	cf ^A 73 °F _{avg} -2.00 "H ₂ O _{avg}		5.117 ✓	cf ^A	75 ✓ °F _{avg}	1.00 ✓ "H ₂ O _{avg}

$$\text{Wet Test Meter } VM_{\text{std}} = 17.65 \times \frac{5.160}{73 + 460} \times \frac{29.94 + \frac{1.00}{13.6}}{75 + 460} \times 0.998 C_f = \frac{5.084}{5.070} \text{ scfm}$$

$$\text{Dry Gas Meter } VM_{\text{std}} = 17.65 \times \frac{5.117}{75 + 460} \times \frac{29.94 + \frac{1.00}{13.6}}{75 + 460} = \frac{5.070}{5.070} \text{ scfm}$$

$$\text{Calibration Factor (C}_{dg}\text{)} = \frac{\text{Wet Test Meter } VM_{\text{std}}}{\text{Dry Gas Meter } VM_{\text{std}}} \quad C_{dg} = \frac{5.084}{5.070} = \frac{1.003}{1.003}$$

QA/QC Check
 Completeness Legibility Accuracy Specifications Reasonableness

Checked by: Ben Sell

10-274B



DRY GAS METER CALIBRATION

Meter Number: T2-4Date: 4-19-10Wet Test Meter No: 2Calibrator: R.Williams

$$\text{Wet Test Meter } VM_{std} = 17.65 \times V_m \quad \frac{P_b + \frac{P_m}{13.6}}{T_m + 460} \times C_f = \text{scfm}$$

$$\text{Dry Test Meter } VM_{std} = 17.65 \times V_m \quad \frac{P_b + \frac{P_m}{13.6}}{T_m + 460} = \text{scfm}$$

Run No: 12150 ✓ "H₂OP_b: 29.94 "HgWet Test Meter C_f: 0.998Control Module Vacuum: 5.0 "HgWet Test Meter

Time	Meter Reading	T _m	P _m	Meter Reading	T _m	Inlet	Outlet	P _m
End 15:00	10.125	73 °F	2.50 "H ₂ O	342.301	80	°F	75 °F	1.50 "H ₂ O
Start 0:00	0.000	73 °F	2.50 "H ₂ O	332.228	77	°F	74 °F	1.50 "H ₂ O
cf ^A = V _m	10.125	cf ^A	73 °F _{avg} 2.50 "H ₂ O _{avg}	10.073 ✓	cf ^A	77 ✓ °F _{avg}	1.50 "H ₂ O _{avg}	

$$\text{Wet Test Meter } VM_{std} = 17.65 \times \frac{10.125}{73} \times \frac{29.94 + \frac{-2.50}{13.6}}{77 + 460} \times 0.998 C_f = \frac{9.944}{9.954} \text{ scfm}$$

$$\text{Dry Gas Meter } VM_{std} = 17.65 \times \frac{10.073}{77} \times \frac{29.94 + \frac{1.50}{13.6}}{77 + 460} = \frac{9.944}{9.954} \text{ scfm}$$

$$\text{Calibration Factor (C}_{dg}\text{)} = \frac{\text{Wet Test Meter } VM_{std}}{\text{Dry Gas Meter } VM_{std}} \quad C_{dg} = \frac{9.944}{9.954} = \frac{1.001}{1.000}$$

QA/QC Check
 Completeness Legibility Accuracy Specifications Reasonableness

Checked by: B. S.

10-274B



DRY GAS METER CALIBRATION

Meter Number: T2-4
 Date: 4-19-10

Wet Test Meter No: 2
 Calibrator: P. Williams

$$\text{Wet Test Meter } VM_{\text{std}} = 17.65 \times V_m \quad \frac{P_b + \frac{P_m}{13.6}}{T_m + 460} \times C_f = \text{scfm}$$

$$\text{Dry Test Meter } VM_{\text{std}} = 17.65 \times V_m \quad \frac{P_b + \frac{P_m}{13.6}}{T_m + 460} = \text{scfm}$$

Run No: 1 @ 2.00 ✓ "H₂O
 Wet Test Meter C_f: 0.998

P_b: 29.94 "Hg
 Control Module Vacuum: 5.0 "Hg

Wet Test MeterDry Gas Meter

Time	Meter Reading	T _m	P _m	Meter Reading	T _m	Inlet	Outlet	P _m
End 12:53	10.150	73 °F	-3.10 "H ₂ O	353.170	82	°F	74 °F	2.00 "H ₂ O
Start 0:00	0.000	73 °F	-3.10 "H ₂ O	343.054	78	°F	75 °F	2.00 "H ₂ O
	10.150 ✓ cf ^A	73.6°F _{avg}	-3.10 "H ₂ O _{avg}	10.114 ✓ cf ^A	78 ✓ °F _{avg}	2.00 "H ₂ O _{avg}		

$$\text{cf}^A = V_m$$

$$\text{Wet Test Meter } VM_{\text{std}} = 17.65 \times \frac{10.150}{73} \quad \frac{29.94 + \frac{-3.10}{13.6}}{73 + 460} \times \frac{0.998}{C_f} = \frac{9.973}{9.992} \text{ scfm}$$

$$\text{Dry Gas Meter } VM_{\text{std}} = 17.65 \times \frac{10.114}{78} \quad \frac{29.94 + \frac{2.00}{13.6}}{78 + 460} = \frac{9.992}{9.997} \text{ scfm}$$

$$\text{Calibration Factor (C}_{dg}\text{)} = \frac{\text{Wet Test Meter } VM_{\text{std}}}{\text{Dry Gas Meter } VM_{\text{std}}} \quad C_{dg} = \frac{9.973}{9.992} = \underline{\underline{0.998}}$$

QA/QC Check
 Completeness Legibility Accuracy Specifications Reasonableness

Checked by: B. SLP

10-274B



DRY GAS METER CALIBRATION

Meter Number: T2-4Wet Test Meter No: 7Date: 4-19-00Calibrator: R. Williams

$$\text{Wet Test Meter } VM_{std} = 17.65 \times V_m \quad \frac{P_b + \frac{P_m}{13.6}}{T_m + 460} \times C_f = \text{scfm}$$

$$\text{Dry Test Meter } VM_{std} = 17.65 \times V_m \quad \frac{P_b + \frac{P_m}{13.6}}{T_m + 460} = \text{scfm}$$

Run No: 1 @ 3.00 ✓ "H₂OP_b: 29.94 "HgWet Test Meter C_f: 0.998Control Module Vacuum: 5.0 "HgWet Test MeterDry Gas Meter

Time	Meter Reading	T _m	P _m	Meter Reading	Inlet T _m	Outlet T _m	P _m
End 10:40	10.150	73 °F	-3.70 "H ₂ O	343.922	85 °F	77 °F	3.00 "H ₂ O
Start 05.00	0.000	73 °F	-3.70 "H ₂ O	353.805	81 °F	74 °F	3.00 "H ₂ O
cf ^A = V _m	10.150 ✓ cf ^A	73 °F _{avg}	-3.70 "H ₂ O _{avg}	10.117 ✓ cf ^A	80 ✓ °F _{avg}	73 °F _{avg}	3.00 "H ₂ O _{avg}

$$\text{Wet Test Meter } VM_{std} = 17.65 \times \frac{10.150}{73} \quad \frac{29.94 + \frac{3.00}{13.6}}{+460} \times 0.998 C_f = \frac{9.959}{9.980} \text{ scfm}$$

$$\text{Dry Gas Meter } VM_{std} = 17.65 \times \frac{10.117}{80} \quad \frac{29.94 + \frac{3.00}{13.6}}{+460} = \frac{9.980}{9.959} \text{ scfm}$$

$$\text{Calibration Factor (C}_{dg}\text{)} = \frac{\text{Wet Test Meter } VM_{std}}{\text{Dry Gas Meter } VM_{std}} \quad C_{dg} = \frac{9.959}{9.980} = \frac{9.959}{9.980} \checkmark$$

QA/QC Check
 Completeness Legibility Accuracy Specifications Reasonableness

Checked by: RE sell

10-274B



DRY GAS METER CALIBRATION

Meter Number: T7-4
 Date: 4-19-10

Wet Test Meter No: 2
 Calibrator: R. Williford

$$\text{Wet Test Meter } VM_{\text{std}} = 17.65 \times V_m \quad \frac{P_b + \frac{P_m}{13.6}}{T_m + 460} \times C_f = \text{scfm}$$

$$\text{Dry Test Meter } VM_{\text{std}} = 17.65 \times V_m \quad \frac{P_b + \frac{P_m}{13.6}}{T_m + 460} = \text{scfm}$$

Run No: 10400 "H₂O P_b: 29.94 "Hg
 Wet Test Meter C_f: 0.998 ✓ Control Module Vacuum: 5.0 "Hg

Wet Test Meter

Time	Meter Reading	T _m	P _m	Met	T _m	Inlet	Outlet	P _m
End	9:14	10.145	73 °F	-4.7 "H ₂ O	374.746	87	78 °F	4.00 "H ₂ O
Start	0:00	0.000	73 °F	-4.7 "H ₂ O	344.417	82	77 °F	4.00 "H ₂ O
		10.145 ✓ cf ^a	73 °F _{avg}	-4.7 "H ₂ O _{avg}	10.129 ✓ cf ^a	81 ✓	78 °F _{avg}	4.00 "H ₂ O _{avg}

cf^a = V_m

$$\text{Wet Test Meter } VM_{\text{std}} = 17.65 \times \underline{10.145} \quad \frac{29.94 + \frac{-4.7}{13.6}}{73 + 460} \times \underline{0.998} C_f = \underline{9.929} \checkmark \text{ scfm}$$

$$\text{Dry Gas Meter } VM_{\text{std}} = 17.65 \times \underline{10.129} \quad \frac{29.94 + \frac{4.00}{13.6}}{81 + 460} = \underline{9.998} \checkmark \text{ scfm}$$

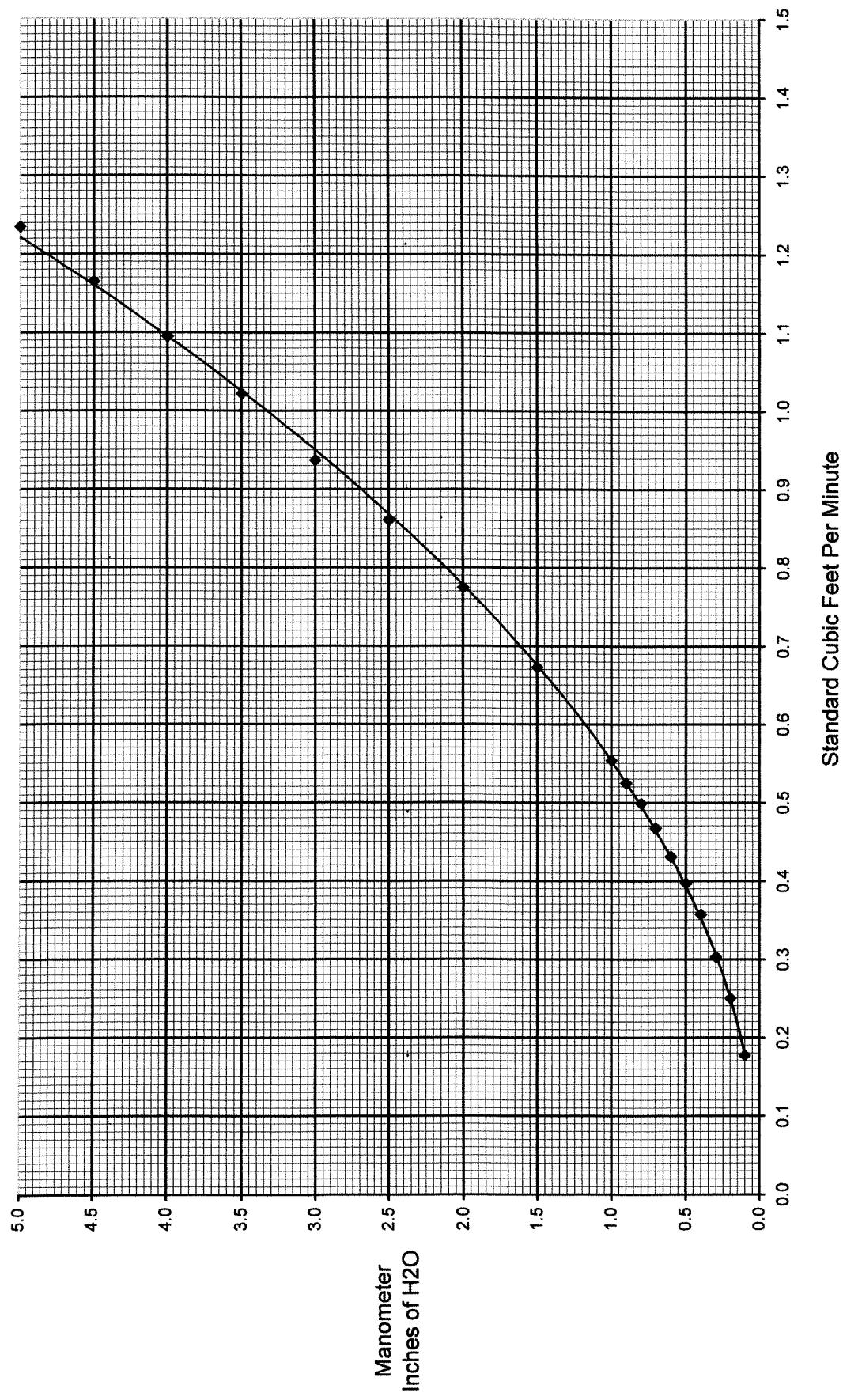
$$\text{Calibration Factor (C}_{dg}\text{)} = \frac{\text{Wet Test Meter } VM_{\text{std}}}{\text{Dry Gas Meter } VM_{\text{std}}} \quad C_{dg} = \frac{9.929}{9.998} = \underline{0.993} \checkmark$$

QA/QC Check
 Completeness Legibility Accuracy Specifications Reasonableness

Checked by: R. Williford

10-274B

STACK UNIT ORIFICE NO: T2-4 DATE: 01/05/10 CALIBRATED BY: Ben Goebel CHECKED BY: Chris Smith





Digital Temperature Indicator No. TZ-4

Calibration Data

Date: 4-19-10

Reference Thermometer No. H-09-1

<u>Media</u>	<u>Time</u>	Reference Thermometer (°F)	DTI (°F)
Ambient Air	<u>8:37</u>	<u>71</u>	<u>71 ✓</u>
Ice Bath	<u>8:40</u>	<u>33</u>	<u>33 ✓</u>
Boiling Water	<u>845</u>	<u>211</u>	<u>211 ✓</u>
Oven	<u>851</u>	<u>251</u>	<u>250 ✓</u>
Oven	<u>9:00</u>	<u>300</u>	<u>301 ✓</u>
Oven	<u>912</u>	<u>351</u>	<u>351 ✓</u>
Oven	<u>920</u>	<u>374</u>	<u>374 ✓</u>
Meter Adjusted?	YES	NO	✓

Calibrator Ry Dell

Office: Houston

QA/QC Check

Completeness Legibility Accuracy Specifications Reasonableness

Checked by: Ry Dell



BAROMETER CALIBRATION

Cherry Hill Office Only

Barometer No. 49-2Date: 5/24/10Time: 1645Barometric Pressure @ Philadelphia Airport @ 36 ft = 30.24- 0.036Absolute Pressure @ Philadelphia Airport = 30.204- 0.014Absolute Pressure @ METCO Cherry Hill @ 50 ft. = 30.19Barometer Reading = 30.19Variation = 0.00Barometer Adjusted? Yes No XCalibrator B. BellQA/QC Check
Completeness / Legibility / Accuracy / Specifications / Reasonableness /Checked by: J. J. J.



APPENDIX D

Field Testing Data

METCO ENVIRONMENTAL

Job Number 10-274 ✓
 Job Name Citego ✓
 Run Number 1
 Unit Wasp FFC-4A ✓
 Date 6-30-10
 Operator Gilbert Biplot ✓
 Sample Box No. 54-2 Meter Box No. 495 ✓

5.20 ✓ Field Data
 Read and record at the start of each test point.

Purge to: 2045-2145 ✓
 Purge time: 28 EPM ✓
 Pitot Leak Check Initial ✓ Final ✓

C Factor 2.103 ✓ to reference.

Initial Leak @ 15.0 "Hg = 0.250 cfm

Final Leak @ 6.0 "Hg = 0.090 cfm

 ΔP_s

Point	Clock Time	Dry Gas Meter, CF	"Pitot" "H ₂ O	Orifice ΔH Desired	Orifice ΔH "H ₂ O Actual	Pump Vacuum "Hg Gauge	Stack Temp °F	Probe Temp °F	Oven Temp °F	Effluent Temp °F	Dry Gas Temp °F Inlet	Dry Gas Temp °F Outlet	Remarks
A 6	1908	291.903	0.53	1.10	1.10	2.5	148	330	323	70	85	83	
5	1910.5	293.48	0.51	1.05	1.05	2.5	148	328	324	57	84	83	
4	1913	295.06	0.52	1.10	1.10	2.5	148	346	331	55	85	83	
3	1915.5	296.82	0.49	1.05	1.05	2.5	148	328	329	54	85	83	
2	1918	298.34	0.40	0.84	0.84	2.5	148	327	326	54	85	84	
1	1920.5	299.69	0.43	0.90	0.90	2.5	148	328	325	55	86	84	
End	1923	301.104	-	-	-	-	-	-	-	-	-	-	
B 6	1931	301.104	0.50	1.05	1.05	2.5	148	326	324	64	84	84	
5	1933.5	302.57	0.50	1.05	1.05	2.5	148	324	328	60	84	84	
4	1936	304.13	0.49	1.05	1.05	2.5	148	328	327	56	84	83	
3	1938.5	305.60	0.43	0.90	0.90	2.5	148	326	325	56	83	83	
2	1941	307.10	0.43	0.90	0.90	2.5	148	327	324	56	83	83	
1	1943.5	308.41	0.43	0.90	0.90	2.5	148	328	325	56	83	82	
End	1946	309.560	-	-	-	-	-	-	-	-	-	-	
C 6	1952	309.560	0.50	1.05	1.05	2.5	148	327	326	70	81	81	
5	1958.5	310.91	0.51	1.05	1.05	2.5	148	323	326	57	81	81	
4	2001	312.37	0.51	1.05	1.05	2.5	148	325	326	57	81	81	
3	2003.5	313.86	0.46	0.97	0.97	2.5	148	326	325	57	81	80	

Pitot Tube Calibration Factor C_p D810 ✓
 Volume Collected V_m 35344 ft³
 Water Collected V_w 201.4 ml
 Time of Test T_t 60 min.
 Stack Pressure P_s -0.32 "H₂O

Pitot Tube No. TY-E-C ✓

Baro. Press. P_b 27.6 "Hg
 Probe Tip Dia. D_n 250 in.
 % CO₂ 14.3 ✓ % CO 0.0
 % O₂ 4.2 ✓ % N₂ 81.5 ✓
 Area Stack A_s 22,167 in²

Barometer No. 47-2 ✓
 Total Volume of Leak Checks After Start: 1 ft
 V_m = Dry Gas Meter Calibration Factor 1.012 x 34725 ✓
 {Dry Gas Meter Reading - ft³ - (T_t - min. X Leak Rate - cfm)}

Impinger Box No. 54-2

			<u>Water Weight Gain</u>	
Impinger 1	Final Weight	<u>950.4</u>	Impinger 1	<u>196.8</u>
	Initial Weight	<u>753.6</u>		
	Increase		Impinger 2	<u>-2.8</u>
Impinger 2	Final Weight	<u>735.8</u>	Impinger 3	<u>3.5</u>
	Initial Weight	<u>738.6</u>		
	Increase		Impinger 4	<u>3.9</u>
Impinger 3	Final Weight	<u>654.4</u>	V _w =	
	Initial Weight	<u>650.9</u>	g SO ₂ = -	
	Increase		V _w =	
Impinger 4	Final Weight	<u>963.0</u>	Impinger 5	
	Initial Weight	<u>959.1</u>		
	Increase		Impinger 6	
Impinger 5	Final Weight		Total	<u>201.4</u> ✓ = V _w
	Initial Weight			
	Increase		P _b = <u>29.66</u> ✓	%CO ₂ = <u>14.3</u> ✓ 6.292
Impinger 6	Final Weight		V _m = <u>35.344</u> ✓	%O ₂ = <u>4.2</u> ✓ 1.344
	Initial Weight		V _w = <u>201.4</u> ✓	%CO = <u>74.3</u> ✓ 00
	Increase		P _m = <u>0.780</u> ✓	%N ₂ = <u>81.5</u> ✓ 22.82
Impinger 7	Final Weight		A _s = <u>22,167</u> ✓	
	Initial Weight		D _n = <u>0.250</u> ✓	
	Increase		T _t = <u>60</u> ✓	
			Avg ΔP = <u>0.466</u> ✓	
			Avg √ΔP = <u>0.682</u> ✓	
			C _p = <u>0.810</u> ✓	
			P _s = <u>-0.32</u> "H ₂ O ✓	<u>27.64</u> ✓ "Hg
			T _m = <u>81</u> °F ✓	<u>541</u> ✓ °R
			T _s = <u>148</u> °F ✓	<u>608</u> ✓ °R

Moisture Content: %M = 0.2171 ✓ M_d = 0.7829 ✓ MW_d = 30.4156 ✓ MW = 27.75 ✓

$$Vm_{std} = 17.65 \frac{P_b + P_m}{13.6} = 17.65 \times 35.344 \left[\frac{29.66 + 0.780}{13.6} \right] = \frac{34.284}{0.571} \frac{\text{ft}^3}{\text{scfm}}$$

$$Vw_{gas} = 0.0472 \times Vw = 0.0472 \times 201.4 = 9.506 \frac{\text{ft}^3}{\text{scfm}}$$

$$\% \text{ Moisture} = \frac{Vw_{gas}}{Vm_{std} + Vw_{gas}} \times 100 = \frac{9.506}{9.506 + 34.284} \times 100 = 21.71 \%$$

$$Vs = 5123.8 \times \frac{0.810}{27.75 \times 29.64} \times \frac{608}{29.64} \times \frac{0.682}{2434} = 2434 \frac{\text{fpm}}{\text{scfm}}$$

ACFM: 374615 374,617SCFM: 253287 ✓24.1

%EA: _____

$$\%I = \frac{1,039 \times 34.284}{0.7829 \times 60 \times 29.64} \times \frac{608}{2434} \times (0.25)^2 = 102.2 \%$$

METCO ENVIRONMENTAL

Job Number 1D-274 ✓
 Job Name City
 Run Number 2
 Unit Wsp FCCU ✓
 Date 7-1-10 ✓
 Operator G. Hart Meter No. 54-2
 Sample box No. Meter Box No. 47-5 ✓

5. 202 Field Data
 Read and record at the start of each test point.

Purge to: 1422
 Purge time: 1522
 Pitot Leak Check Initial ✓ Final ✓

Pitot Tips Damaged During Test? Yes (No)

Point	Clock Time	Dry Gas Meter, CF	"Pitot" "H ₂ O	Orifice ΔH "H ₂ O Desired	Orifice ΔH "H ₂ O Actual	Vacuum "Hg Gauge	Pump "Hg Gauge	Stack Temp °F	Probe Temp °F	Oven Temp °F	Effluent Temp °F	Dry Gas Temp °F Inlet	Dry Gas Temp °F Outlet	Remarks
A ₁ s	1208	327.725	0.50	1.05	1.05	3.0	146	327	326	75	84	85		
S	1210.5	329.21	0.50	1.05	1.05	3.0	147	326	325	68	84	84		
4	1213	320.69	0.47	0.94	0.94	3.0	147	328	327	64	84	84		
3	1215.5	332.16	0.47	0.91	0.91	3.0	147	327	326	63	84	85		
2	1218	333.62	0.43	0.90	0.90	2.5	147	325	327	62	85	85		
1	1220.5	335.00	0.43	0.90	0.90	2.5	147	326	329	61	85	85		
End	1223	336.432	-	-	-	-	-	-	-	-	-	-		
B ₆	1237	336.432	0.50	1.05	1.05	3.0	147	328	327	74	84	85		
5	1239.5	338.29	0.46	0.97	0.97	3.0	147	326	325	64	85	85		
4	1242	339.30	0.46	0.97	0.97	3.0	147	328	326	62	83	85		
3	1241.5	340.50	0.46	0.97	0.97	3.0	147	327	325	60	83	85		
2	1247	341.45	0.46	0.97	0.97	3.0	147	326	326	59	82	86		
1	1249.5	343.32	0.46	0.97	0.97	3.0	147	328	327	57	82	86		
End	1252	344.44	-	-	-	-	-	-	-	-	-	-		
C ₆	1303	344.444	0.49	1.05	1.05	3.0	147	327	326	74	85	86		
S	1305.5	345.75	0.48	1.03	1.03	3.0	147	328	325	65	85	86		
4	1308	347.20	0.45	0.95	0.95	3.0	147	327	326	61	86	86		
3	1310.5	348.52	0.45	0.95	0.95	3.0	147	326	328	61	87	86		

Pitot Tube Calibration Factor C_p 0.810 ft³
 Volume Collected V_m 33.751 ft³
 Water Collected V_w 216.3 ml
 Time of Test T_t 60 min.
 Stack Pressure P_s -0.32 "H₂O

QA/QC Check / Legibility / Completeness /

Pitot Tube No. 74-E5K-6
 Baro. Press. P_b 29.94 "Hg
 Probe Tip Dia. D 2.50 in.
 % CO₂ 14.4 % CO
 % O₂ 3.6 % O₂

Accuracy / Reasonableness / Specifications /

Barometer No. 49-2 Probe Tip No. 10-274-II
 Total Volume of Leak Checks After Start: _____ ft³
 V_m = Dry Gas Meter Calibration Factor 1.5/2 X 32.351
 Area Stack A_s 2.2, 16.7 in²
 {Dry Gas Meter Reading - ft³ - (T_t - min. X Leak Rate - cfm)}

Checked by: _____

Version 2
 1 February 2008

Impinger Box No. 54-2902.8JC
805.2
720.4Water Weight Gain

Impinger 1	Final Weight	<u>805.2</u>
	Initial Weight	<u>720.4</u>
	Increase	

Impinger 1 182.4

Impinger 2	Final Weight	<u>788.6</u>
	Initial Weight	<u>764.3</u>
	Increase	

Impinger 2 24.3

Impinger 3	Final Weight	<u>655.8</u>
	Initial Weight	<u>633.3</u>
	Increase	

Impinger 3 2.5

Impinger 4	Final Weight	<u>1014.4</u>
	Initial Weight	<u>1007.3</u>
	Increase	

Impinger 4 7.1

Impinger 5	Final Weight	<u> </u>
	Initial Weight	<u> </u>
	Increase	

$$V_w = \\ g SO_2 = - \\ V_v =$$

Impinger 5

Impinger 6	Final Weight	<u> </u>
	Initial Weight	<u> </u>
	Increase	

$$P_b = \frac{29.94}{13.6} \checkmark \\ V_m = 33.751 \checkmark \\ V_w = 216.3 \checkmark \\ P_m = 0.982 \checkmark \\ \% CO_2 = 14.4 \checkmark 6.336 \\ \% O_2 = 3.6 \checkmark 1.152 \\ \% CO = 0 \checkmark \\ \% N_2 = 82.0 \checkmark 22.96$$

$$A_n = 22,167 \checkmark \\ D_n = 0.250 \checkmark \\ T_i = 60$$

Impinger 7	Final Weight	<u> </u>
	Initial Weight	<u> </u>
	Increase	

$$Avg \Delta P = 0.466 \checkmark \\ Avg \sqrt{\Delta P} = 0.683 \checkmark \\ C_p = \frac{0.820}{0.810} \text{ kg} \\ P_a = -0.32 / H_2O \\ T_m = 85 \checkmark ^\circ F \\ T_s = 147 \checkmark ^\circ F \\ \% Hg = 29.92 \checkmark \\ \% R = 545 \checkmark \\ \% R = 607 \checkmark$$

Moisture Content: %M = 23.73 ✓ M_d = 0.7627 ✓ MW_d = 30.448 ✓ MW = 27.49 ✓

$$Vm_{std} = 17.65 \quad Vm \left[\frac{P_b + \frac{P_m}{13.6}}{T_m + 460} \right] = 17.65 \times 33.751 \left[\frac{29.94 + \frac{0.982}{13.6}}{85 + 460} \right] = \frac{32.804}{0.547} \frac{ft^3}{scfm}$$

$$Vw_{gas} = 0.0472 \times Vw = 0.0472 \times \frac{216.3}{10.209} = \frac{10.209}{10.209} \frac{ft^3}{ft^3}$$

$$\% \text{ Moisture} = \frac{Vw_{gas}}{Vm_{std} + Vw_{gas}} \times 100 = \frac{10.209}{10.209 + 32.804} \times 100 = \frac{23.73}{53.01} \checkmark \%$$

$$V_s = 5123.8 \times \frac{0.810}{0.820} \sqrt{\frac{607}{27.49} \times \frac{0.683}{29.92}} = \frac{2480}{2480} \frac{ft^3}{min}$$

$$ACFM: \frac{374,859}{381,801} \frac{ft^3}{min}$$

$$SCFM: \frac{249,546}{254,204} \frac{ft^3}{min}$$

$$\% EA: \frac{19.9}{19.9}$$

$$\% I = \frac{1,039 \times 32.804 \times 607}{2480 \times 0.7627 \times 60 \times 29.92 \times (0.250)^2} = \frac{975}{95} \frac{kg}{kg} \checkmark \\ \% EA = 99.30\%$$

Run Number 2
 Unit Wasp Fuel
 Date 17-1-10

FIELD DATA

 ΔP_s P_m T_m T_s Dry Gas Temp °F
Outlet

Point	Clock Time	Dry Gas Meter, CF	"Pitot" "H ₂ O	Orifice ΔH "H ₂ O Desired	Orifice ΔH "H ₂ O Actual	Pump Vacuum "Hg Gauge	Stack Temp °F	Probe Temp °F	Oven Temp °F	Effluent Temp °F	Dry Gas Temp °F Inlet	Dry Gas Temp °F Outlet	Remarks
2	1313	349.92	0.45	0.55	0.55	3.0	147	327	328	61	87	86	
1	135.5	351.32	0.46	0.47	0.47	3.0	147	328	327	60	90	87	
End	1318	352.62	-	-	-	-	-	-	-	-	-	-	
D6	1321	352.662	0.47	0.49	0.49	3.0	147	327	326	77	88	87	
5	1333.5	353.87	0.47	0.49	0.49	3.0	147	329	327	62	85	87	
4	1334	355.33	0.46	0.47	0.47	3.0	147	327	326	56	85	86	
3	1338.5	356.87	0.47	0.49	0.49	3.0	147	328	327	54	87	86	
2	1341	358.27	0.47	0.49	0.49	3.0	147	329	326	55	87	87	
1	1343.5	359.32	0.47	0.49	0.49	3.0	147	326	327	54	88	87	
End	1346	361.076	-	-	-	-	-	-	-	-	-	-	

METCO ENVIRONMENTAL

Job Number 10-274 ✓
 Job Name Citgo
 Run Number 3
 Unit 1120sp FCU ✓
 Date 7-1-10
 Operator G. Bush Morri's ✓
 Sample box No. S4-9 Meter Box No. 47-5 ✓

55/202 ✓

Read and record at the start of each test point.

Purge to: 1705 ✓
 Purge time: 1805 ✓
 Pitot Leak Check Initial ✓ Final ✓

 ΔP_s P_m T_s T_m

Point	Clock Time	Dry Gas Meter, CF	"Pitot" "H ₂ O	Orifice ΔH "H ₂ O Desired	Orifice ΔH "H ₂ O Actual	Pump Vacuum "Hg Gauge	Stack Temp °F	Probe Temp °F	Oven Temp °F	Effluent Temp °F	Dry Gas Temp °F Inlet	Dry Gas Temp °F Outlet	Remarks
A1	150225	361.790	0.45	0.35	0.35	1.3	147	326	327	77	88	88	
5	150225	363.03	0.45	0.35	0.35	4.0	147	325	328	74	88	88	
4	1505	364.44	0.45	0.35	0.35	4.0	147	326	329	68	87	88	
3	1507.5	365.81	0.46	0.37	0.37	4.0	147	325	326	64	88	87	
2	1510	367.32	0.46	0.37	0.37	4.0	147	324	327	63	87	87	
1	1512.5	368.71	0.46	0.37	0.37	4.0	147	326	327	62	89	88	
E ₁	1515	370.042	-	-	-	-	-	-	-	-	-	-	
B6	1532	370.042	0.47	0.39	0.39	4.0	146	327	328	76	88	88	
5	1534.5	371.34	0.47	0.39	0.39	4.0	146	328	326	66	87	88	
4	1537	372.73	0.47	0.39	0.39	4.0	146	327	325	61	90	88	
3	1539.5	374.15	0.48	1.00	1.00	4.0	147	326	328	59	70	88	
2	1542	375.63	0.48	1.00	1.00	4.0	147	327	326	57	90	88	
1	1544.5	376.95	0.46	0.37	0.37	4.0	147	327	325	55	91	88	
E ₂	1547	378.474	-	-	-	-	-	-	-	-	-	-	
6	1555	378.174	0.46	0.37	0.37	4.5	146	328	326	73	90	88	
5	1557.5	379.90	0.47	0.39	0.39	4.5	147	326	327	64	91	89	
4	1600	381.31	0.47	0.39	0.39	4.5	147	327	326	62	91	90	
3	1602.5	382.64	0.49	0.33	0.33	4.5	147	326	322	61	90	89	

Pitot Tube Calibration Factor C_p 0.810
 Volume Collected V_m 33.542 ft³
 Water Collected V_w 211.3 ml
 Time of Test T_t 60 min.
 Stack Pressure P_s -0.34 "H₂O

QA/QC Check ✓ Completeness ✓ Legibility ✓ Accuracy ✓ Reasonableness ✓ Specifications ✓ Checked by: _____

Pitot Tube No. 49-2 ✓ Probe Tip No. 10-274-II ✓
 Baro. Press. B_a 29.92 "Hg Total Volume of Leak Checks After Start: $\frac{V_m}{R}$ ft³
 Probe Tip Dia. D_p 0.250 in. V_m = Dry Gas Meter Calibration Factor 10.2 ✓ X 32.144 ✓
 % CO₂ 14.5 % CO 0 ✓ Area Stack A_s 22.167 in² ✓
 % O₂ 3.7 % N₂ 81.5 ✓ (Dry Gas Meter Reading - ft³ - (T_t - min. X Leak Rate / cfm))

Version 2
 1 February 2008

Impinger Box No. 54-4

<u>Water Weight Gain</u>		
Impinger 1	Final Weight Initial Weight Increase	<u>897.5</u> <u>702.8</u>
Impinger 2	Final Weight Initial Weight Increase	<u>753.4</u> <u>750.7</u>
Impinger 3	Final Weight Initial Weight Increase	<u>735.3</u> <u>731.1</u>
Impinger 4	Final Weight Initial Weight Increase	<u>968.8</u> <u>959.1</u>
Impinger 5	Final Weight Initial Weight Increase	<u>29.92</u> ✓ <u>33.542</u> ✓ <u>21.3</u>
Impinger 6	Final Weight Initial Weight Increase	<u>0.979</u> ✓ <u>0.465</u> ✓ <u>0.682</u> ✓
Impinger 7	Final Weight Initial Weight Increase	<u>-0.34</u> ✓ <u>84</u> ✓ °F <u>147</u> ✓ °F
Total		<u>211.3</u> ✓ = <u>V_w</u>

$P_b = 29.92 \checkmark$ $\%CO_2 = 14.5 \checkmark$
 $V_m = 33.542 \checkmark$ $\%O_2 = 83.7 \checkmark$
 $V_w = 21.3$ $\%CO = 0.0$
 $P_m = 0.979 \checkmark$ $\%N_2 = 81.8 \checkmark$
 $A_n = 22,167 \checkmark$
 $D_n = 0.250 \checkmark$
 $T_i = 60 \checkmark$
 $C_p = 0.810 \checkmark$
 $P_i = -0.34 \text{ H}_2\text{O}$ $29.90 \checkmark \text{ Hg}$
 $T_m = 84 \checkmark \text{ °F}$ $549 \checkmark \text{ °R}$
 $T_i = 147 \checkmark \text{ °F}$ $607 \checkmark \text{ °R}$

$$\text{Moisture Content: } \%M = \frac{23.57}{23.57} \checkmark \quad M_d = \frac{0.7643}{0.7643} \checkmark \quad MW_d = \frac{30.465}{30.465} \checkmark \quad MW = \frac{27.53}{27.53} \checkmark$$

$$Vm_{std} = 17.65 \quad Vm \left[\frac{P_b + \frac{P_m}{13.6}}{\frac{T_m + 460}{T_i + 460}} \right] = 17.65 \times \frac{29.92 + \frac{0.979}{13.6}}{\frac{84 + 460}{607 + 460}} = \frac{32.342}{0.537} \frac{\text{ft}^3}{\text{scfm}}$$

$$Vw_{gas} = 0.0472 \times Vw = 0.0472 \times \frac{211.3}{27.53} = \frac{9.973}{27.53} \checkmark \text{ ft}^3$$

$$\% \text{ Moisture} = \frac{Vw_{gas}}{Vm_{std} + Vw_{gas}} \times 100 = \frac{9.973}{9.973 + 32.342} \times 100 = \frac{23.57}{56.31} \checkmark \%$$

$$V_i = 5123.8 \times 0.810 \sqrt{\frac{607}{29.90} \times \frac{0.682}{27.53}} = \frac{2431}{2431} \text{ fpm}$$

ACFM: 374,164 ✓

$$\%I = \frac{1,039 \times 32.342 \times 607}{2431 \times 0.7643 \times 29.90 \times 60 \times (0.250)^2} = \frac{97.9}{97.9} \% \checkmark$$

SCFM: 249,542 ✓%EA: 20.4

Run Number 3
 Unit 1005P FCCU
 Date 7-1-10

FIELD DATA

 ΔP_s P_m T_m

Remarks

Point	Clock Time	Dry Gas Meter, CF	"Pitot" "H ₂ O	Orifice "H ₂ O Desired	Orifice "H ₂ O Actual	Pump Vacuum "Hg Gauge	Stack Temp °F	Probe Temp °F	Oven Temp °F	Effluent Temp °F	Dry Gas Temp °F Inlet	Dry Gas Temp °F Outlet	
2	1605	384.02	0.44	0.93	0.93	4.5	147	325	325	61	91	87	
1	1607.5	385.23	0.43	0.90	0.90	4.5	147	326	327	61	89	88	
End	1610	386.525	-	-	-	-	-	-	-	-	-	-	
D6	1621	386.525	0.50	1.05	1.05	5.0	149	325	327	73	88	86	
S	1623.5	388.04	0.50	1.05	1.05	5.0	149	326	328	63	85	87	
4	1626	389.42	0.50	1.05	1.05	5.0	150	326	329	60	90	88	
3	1628.5	390.73	0.50	1.05	1.05	5.5	150	327	326	59	92	88	
2	1631	392.14	0.52	1.10	1.10	6.0	150	327	324	59	92	90	
1	1633.5	393.72	0.37	0.78	0.78	6.0	149	328	325	61	91	90	
End	1636	394.934	-	-	-	-	-	-	-	-	-	-	

METCO ENVIRONMENTAL

Job Number 10-274 ✓
 Job Name C1150 ✓
 Run Number 1
 Unit 101 ✓ FCCV ✓
 Date 6/10/10 ✓
 Operator Starkley/Morris/C.J. Amm ✓
 Sample box No. 7 Meter Box No. T2-4 ✓

OTM 28 ✓ Field Data

Read and record at the start of each test point.

Purge to: 2045-2145 ✓
 Purge time: 28 LPM ✓
 Pitot Leak Check Initial ✓ Final ✓

Ambient Temp. F 75 ✓
 Assumed Moisture % 24.14 ✓
 Probe Length 2.10 28 ✓ to reference.
 C Factor 2.10 28 ✓ "Hg = 0.00 2 ✓ cfm
 Initial Leak @ 16.0 "Hg = 0.00 1 ✓ cfm
 Final Leak @ 18.0 "Hg = 0.00 1 ✓ cfm

 ΔP_s

Point	Clock Time	Dry Gas Meter, CF	"Pitot" "H ₂ O	Orifice ΔH "H ₂ O Desired	Orifice ΔH "H ₂ O Actual	Pump Vacuum "Hg Gauge	Stack Temp °F	Probe Temp °F	Oven Temp °F	Effluent Temp °F	Dry Gas Temp °F Inlet	Dry Gas Temp °F Outlet	Remarks
06	1908	208.927	0.455	0.95	4.0	149	324	328	73	86	84	325°F ± 3°F	
5	1905	210.23	0.50	1.05	4.0	145	320	320	73	86	84		
4	1913	211.80	0.53	1.10	4.5	149	328	324	61	85	84		
3	1915.5	213.25	0.36	0.76	4.0	149	328	326	62	85	84		
2	1918	214.55	0.36	0.76	4.0	143	328	326	62	83	84		
1	1920.5	215.59	0.30	0.63	4.63	149	328	329	62	85	84		
ENR	1923	216.573	-	-	-	-	-	-	-	-	-		
C6	1931	216.573	0.47	0.94	4.0	149	324	328	62	86	84		
5	1933.5	217.45	0.49	1.00	4.00	150	326	328	63	86	85		
4	1936	219.13	0.48	1.00	4.00	150	328	328	64	85	84		
3	1938.5	220.65	0.46	0.97	0.97	130	326	329	64	85	84		
2	1941	222.14	0.32	0.67	0.67	150	326	329	63	86	84		
1	1943.5	223.21	0.30	0.63	3.5	150	323	328	63	86	84		
ENR	1946	224.357	-	-	-	-	-	-	-	-	-		
BL	1956	224.357	0.48	1.00	4.5	149	324	328	65	81	84		
5	1958.5	225.87	0.41	1.00	4.5	149	326	324	52	81	81		
4	1960	227.00	0.47	0.99	0.99	144	326	327	52	81	81		
3	1960.9	228.47	0.40	0.84	0.84	146	327	328	53	81	81		

Pitot Tube Calibration Factor C_p 0.820 ✓
 Volume Collected V_m 148.31.863 ft³
 Water Collected V_w 210 ✓ ml
 Time of Test T_t 60 ✓ min.
 Stack Pressure P_s -0.32 "H₂O ✓

Pitot Tube No. T4-E-8 ✓
 Baro. Press. P_b 24.66 "Hg
 Probe Tip Dia. D_n 0.25" ✓ in.
 % CO₂ 14.3 ✓ % CO 6.0 ✓
 % O₂ 11.2 ✓ % N₂ 81.5 ✓
 Area Stack A_s 22167 in²

Barometer No. 49-2 ✓ Probe Tip No. 10-274-T ✓
 Total Volume of Leak Checks After Start: _____ ft³
 V_m = Dry Gas Meter Calibration Factor $\frac{1.000}{1.000} \times 31.863$ ✓
 (Dry Gas Meter Reading ft³ - (T_t min. X Leak Rate in³ cfm))

Impinger Box No. 7

Impinger 1	Final Weight Initial Weight Increase	<u>737.5</u> 811.1	Water Weight Gain	Impinger 1	<u>197.9</u>
Impinger 2	Final Weight Initial Weight Increase	<u>668.0</u>		Impinger 2	<u>1.6</u>
Impinger 3	Final Weight Initial Weight Increase	<u>737.5</u>	$V_w =$ $g SO_2 = -$ $V_w =$	Impinger 3	<u>-0.9</u>
Impinger 4	Final Weight Initial Weight Increase	<u>938.8</u>		Impinger 4	<u>11.4</u>
Impinger 5	Final Weight Initial Weight Increase	<u>927.4</u>		Impinger 5	
Impinger 6	Final Weight Initial Weight Increase			Impinger 6	
Impinger 7	Final Weight Initial Weight Increase			Impinger 7	
Total		<u>210</u> ✓	$= V_w$		
				$P_b = \frac{29.66}{21.440}$ ✓	$\% CO_2 = \frac{14.3}{31.863}$ ✓
				$V_m = \frac{21.440}{29.66}$ ✓	$\% O_2 = \frac{4.2}{31.863}$ ✓
				$V_w = \frac{210}{29.66}$ ✓	$\% CO = \frac{0.0}{29.66}$ ✓
				$P_m = \frac{0.881}{0.420}$ ✓	$\% N_2 = \frac{81.5}{29.66}$ ✓
				Avg $\Delta P = \frac{0.420}{0.646}$ ✓	$A_s = \frac{22167}{29.66}$ ✓
				$C_p = \frac{0.820}{0.646}$ ✓	$D_n = \frac{0.250}{29.66}$ ✓
				$P_s = \frac{-0.32}{82}$ ✓ H_2O ✓	$T_t = \frac{60}{542}$ ✓ $^{\circ}R$
				$T_m = \frac{82}{29.66}$ ✓ $^{\circ}F$	$MW_d = \frac{27.438}{29.66}$ ✓ $^{\circ}R$
				$T_s = \frac{149}{29.66}$ ✓ $^{\circ}F$	$MW = \frac{27.438}{29.66}$ ✓ $^{\circ}R$
Moisture Content:		$\% M = \frac{24.32}{24.25}$ ✓	$M_d = \frac{0.7568}{0.7575}$ ✓	$MW_d = \frac{31.863}{30.46}$ ✓	30.843 ✓
					$\frac{30.966}{0.516}$ scfm ✓
					0.514 ✓
$V_{m_{std}}$	$17.65 V_m \left[\frac{P_b + \frac{P_m}{13.6}}{T_m + 460} \right] = 17.65 \times \frac{29.66}{21.440} \left[\frac{29.66 + \frac{0.881}{13.6}}{82 + 460} \right] = \frac{30.966}{0.516}$ scfm ✓				
$V_{w_{gas}}$	$0.0472 \times V_w = 0.0472 \times \frac{210}{9.912} = 9.912$ ✓ sft^3				
% Moisture	$\frac{V_{w_{gas}}}{V_{m_{std}} + V_{w_{gas}}} \times 100 = \frac{9.912}{9.912 + \frac{30.966}{0.516}} \times 100 = \frac{24.25}{30.843} \%$ ✓				
V_s	$5123.8 \times \frac{0.820}{609} \times \frac{609}{29.64} \times \frac{0.646}{27.44} = 2349$ fpm ✓				
%I	$\frac{1.039 \times 30.966}{30.843} \times 609 = \frac{99.0}{27.44} \%$ ✓				

$$V_{w_{gas}} = 0.0472 \times V_w = 0.0472 \times \frac{210}{9.912} = 9.912 \text{ sft}^3$$

$$\% \text{ Moisture} = \frac{V_{w_{gas}}}{V_{m_{std}} + V_{w_{gas}}} \times 100 = \frac{9.912}{9.912 + \frac{30.966}{0.516}} \times 100 = \frac{24.25}{30.843} \%$$

$$V_s = 5123.8 \times \frac{0.820}{609} \times \frac{609}{29.64} \times \frac{0.646}{27.44} = 2349 \text{ fpm}$$

$$\% I = \frac{1.039 \times 30.966}{30.843} \times 609 = \frac{99.0}{27.44} \%$$

$$\text{ACFM: } \frac{361543}{235.905} \text{ fpm} \checkmark$$

$$\text{SCFM: } \frac{236123}{235.905} \text{ fpm} \checkmark$$

$$\% EA: \frac{24.1}{10-274B}$$

Run Number
Unit
Date

4847 FCCU
10/30/10

0 TM 28 FIELD DATA

ΔP_s

Weight FCCU

10/30/10

T_m

T_m

AP_s

Remarks

Point	Clock Time	Dry Gas Meter, CF	"Pilot" "H ₂ O	Orifice ΔH "H ₂ O Desired	Orifice ΔH "H ₂ O Actual	Pump Vacuum "Hg Gauge	Stack Temp °F	Probe Temp °F	Oven Temp °F	Effluent Temp °F	Dry Gas Temp °F Inlet	Dry Gas Temp °F Outlet	Remarks
B 2	2006	224.73	0.38	0.80	0.80	4.0	146	326	328	59	79	80	
1	2008.5	230.92	0.30	0.63	0.63	3.5	149	322	325	60	79	80	
END	2011	232.147	—	—	—	—	—	—	—	—	—	—	
46	2019	232.147	0.49	1.05	1.05	4.5	149	327	328	60	75	75	
5	2021.5	233.51	0.48	1.00	1.00	4.5	149	322	327	52	75	75	
4	2024	234.94	0.46	0.97	0.97	4.5	149	325	325	44	75	75	
3	2026.5	236.52	0.38	0.86	0.80	4.0	148	326	329	48	76	75	
2	2024	238.00	0.38	0.80	0.66	4.0	148	327	328	48	76	75	
1	2021.5	239.14	0.36	0.76	0.76	4.5	148	328	328	49	77	75	
END	2034	240.790	—	—	—	—	—	—	—	—	—	—	

METCO ENVIRONMENTAL

10-274 ✓

 Job Number
 Job Name
 Run Number
 Unit

Date

Operator

Sample box No.

OTM 28 Field Data

Test RICU ✓
 2/1/10 ✓
 Starkey/Merritt Estimating
 Meter Box No. T2-4 ✓
 APs ✓
 T_s ✓
 ΔP_s ✓
 Read and record at the start of each test point.

Purge to: 1422 ✓

Purge time: 1522 ✓

Pitot Leak Check Initial ✓ Final ✓

Ambient Temp. °F 76 ✓

Assumed Moisture % 100 ✓

Probe Length 10 ✓

C Factor 2.1028 ✓

to reference.

Initial Leak @ 16.0 "Hg = 0.005 cfm

Final Leak @ 8.0 "Hg = 0.005 cfm

Pitot Tips Damaged During Test? Yes No

Point	Clock Time	Dry Gas Meter, CF	"Pilot" "H ₂ O	Orifice ΔH "H ₂ O Desired	Pump Vacuum "Hg Gauge	Stack Temp °F	Probe Temp °F	Oven Temp °F	Effluent Temp °F	Dry Gas Temp °F Inlet	Dry Gas Temp °F Outlet	Remarks
D6	12:08	241,396	0.50	1.05	1.05	41.5	148	322	328	67	86	85
5	12:05	243,110	0.50	1.05	1.05	41.5	148	328	322	60	82	85
4	12:13	244,470	0.48	1.00	1.00	41.5	148	321	326	60	84	85
3	12:15,5	245,750	0.46	0.97	0.97	41.0	148	323	327	59	84	85
2	12:18	247,810	0.32	0.67	0.67	40.0	148	324	328	55	84	85
1	12:20,5	248,310	0.32	0.67	0.67	41.0	148	329	320	60	84	85
END	12:23	249,578	-	-	-	-	148	-	-	-	-	-
C	12:37	249,578	0.50	1.05	1.05	41.5	148	332	324	61	84	85
5	12:39,5	250,880	0.49	1.00	1.00	41.5	148	326	334	61	83	85
4	12:42	252,020	0.48	1.00	1.00	41.5	148	326	334	61	87	85
3	12:44,5	253,739	0.47	0.99	0.99	51.0	148	326	336	62	87	85
2	12:47	254,920	0.32	0.67	0.67	41.0	148	328	338	62	88	85
1	12:49,5	256,140	0.32	0.67	0.67	41.0	148	328	326	60	88	86
END	12:52	257,427	-	-	-	-	148	-	-	-	-	-
B6	13:03	257,427	0.52	1.10	1.10	51.0	148	328	326	61	87	86
5	13:05,5	259,040	0.50	1.05	1.05	41.5	148	327	324	61	88	86
4	13:08	260,350	0.46	0.97	0.97	41.5	148	327	322	60	88	86
3	13:10,5	261,550	0.46	0.97	0.97	41.5	147	328	323	58	87	86

Pitot Tube Calibration Factor C_p 0.823 Pitot Tube No. T4-E_{SC}-8 ✓
 Baro. Press. P_b 25.94 ft³ "Hg ✓
 Volume Collected V_m 32.82 ft³ ✓
 Water Collected V_w 200.0 ml ✓
 Time of Test T_t 60 min. ✓
 Stack Pressure P_s - 0.32 "H₂O ✓

QA/QC Check ✓ Legibility ✓ Completeness ✓ Accuracy ✓ Specifications ✓ Reasonableness ✓ Checked by: ✓

Barometer No. 49-2 ✓ Probe Tip No. 10-274-I ✓
 Total Volume of Leak Checks After Start: $\frac{V_m}{P_s}$ ft³ ✓
 Probe Tip D_d, D_h 0.250 in. ✓
 % CO₂ 14.4 % CO 82 ✓
 % O₂ 3.6 % N₂ 82.0 ✓
 (Dry Gas Meter Reading - ft³ - (T_t - min. X Leak Rate - cfm))

Version 2
 1 February 2008

Impinger Box No. 7

			<u>Water Weight Gain</u>			
Impinger 1	Final Weight	<u>805.2</u>		Impinger 1	<u>191.9</u>	
	Initial Weight	<u>618.3</u>				
	Increase			Impinger 2	<u>-0.4</u>	
Impinger 2	Final Weight	<u>667.9</u>		Impinger 3	<u>-0.4</u>	
	Initial Weight	<u>668.3</u>		Impinger 4	<u>9.8</u>	
	Increase			Impinger 5		
Impinger 3	Final Weight	<u>736.1</u>	$V_w =$	Impinger 5		
	Initial Weight	<u>736.5</u>	$g SO_2 =$	Impinger 6		
	Increase		$V_w =$	Impinger 6		
Impinger 4	Final Weight	<u>964.0</u>		Impinger 7		
	Initial Weight	<u>954.2</u>		Total	<u>200.9</u>	$\checkmark = V_w$
	Increase					
Impinger 5	Final Weight		$P_b = \frac{29.94}{32.012} 31.914$	%CO ₂	<u>14.4</u>	\checkmark
	Initial Weight		$V_m = \frac{TF}{32.012}$	%O ₂	<u>3.6</u>	\checkmark
	Increase		$V_w = \frac{202.9}{32.012}$	%CO	<u>0.2</u>	\checkmark
Impinger 6	Final Weight		$P_m = \frac{TF}{32.012} 0.905$	%N ₂	<u>82.0</u>	\checkmark
	Initial Weight		Avg ΔP = <u>0.431</u>	A _n	<u>22.167</u>	\checkmark
	Increase		Avg √ΔP = <u>0.650</u>	D _n	<u>0.250</u>	\checkmark
Impinger 7	Final Weight		C _p = <u>0.820</u>	T _i	<u>60</u>	\checkmark
	Initial Weight		P _b = <u>-0.32</u> "H ₂ O			
	Increase		T _m = <u>TF 88.86</u> °F		29.92 "Hg	\checkmark
			T _w = <u>148</u> °F		TF 54.6 °R	\checkmark
					54.6 °R	\checkmark
					60.8 °R	\checkmark
Moisture Content:		<u>23.45</u>	<u>0.7655</u>			
		<u>%M = 23.44</u> °F	M _d = <u>0.7655</u> °F	MW _d = <u>30.448</u>	\checkmark	MW = <u>27.53</u> \checkmark

$$Vm_{std} = 17.65 \quad Vm \left[\frac{P_b + \frac{P_m}{13.6}}{\frac{T_m + 460}{32.012}} \right] = 17.65 \times \frac{31.914}{\frac{29.94 + \frac{0.905}{0.516}}{32.012 + 460}} = \frac{30.956}{0.516} \text{ scfm} \quad \checkmark$$

$$Vw_{gas} = 0.0472 \times Vw = 0.0472 \times \frac{200.9}{27.53} = 9.482 \text{ scft}^3$$

$$\% \text{ Moisture} = \frac{Vw_{gas}}{Vm_{std} + Vw_{gas}} \times 100 = \frac{9.482}{30.956 \frac{30.956}{32.012} + 9.482} \times 100 = \frac{23.44}{23.45} \text{ %}$$

$$V_i = 5123.8 \times \frac{608}{\sqrt{27.53 \times 29.92}} \times 0.653 = 2357 \text{ lpm} \quad \checkmark$$

ACFM: 362854 \checkmark SCFM: 2412120 242,089

$$\%I = \frac{1,039 \times 30.956 \times 608}{2357 \times 6.7657 \times 60 \times 29.92 \times (0.250)^2} = 96.6 \% \quad \checkmark$$

%EA: 19.9

07M 28 FIELD DATA

Run Number 2
 Unit Wet FCCU
 Date 7/17/00

Point	Clock Time	Dry Gas Meter, CF	"Pitot" "H ₂ O	Orifice ΔH "H ₂ O Desired	Orifice ΔH "H ₂ O Actual	Pump Vacuum "Hg Gauge	Stack Temp °F	Probe Temp °F	Oven Temp °F	Effluent Temp °F	Dry Gas Temp °F Inlet	Dry Gas Temp °F Outlet	Remarks
2	13/3	263,21	0,33	0,69	0,69	41,0	147	328	326	57	87	86	
1	1315,5	264,42	0,28	0,59	0,59	3,5	147	328	326	57	87	88	
END	1318	265,351	-	-	-	-	-	-	-	-	-	-	
A6	1331	265,351	0,52	1,10	1,10	5,0	148	322	325	58	87	86	
5	1333,5	266,85	0,50	1,05	1,05	3,0	148	322	324	58	88	88	
4	1336	268,10	0,48	1,00	1,00	4,5	148	324	324	59	88	88	
3	1338,5	269,78	0,46	0,97	0,97	4,5	147	328	325	59	88	88	
2	1341	270,93	0,40	0,84	0,84	4,5	148	326	327	59	88	88	
1	1343,5	271,18	0,26	0,59	0,59	3,5	146	326	327	59	88	88	
END	1346	273,310	-	-	-	-	-	-	-	-	-	-	

METCO ENVIRONMENTAL

Job Number 10-274 ✓
 Job Name Cdgs
 Run Number 3
 Unit West FCCU ✓
 Date 6/1/10
 Operator Sherker/Merris/Cohrak ✓
 Sample box No. BRI Meter Box No. 172-4 ✓

SB/05FM 28 ✓
 Field Data

Read and record at the start of each test point.

Purge to: 1705 ✓
 Purge time: 1805 ✓
 Pitot Leak Check Initial ✓ Final ✓

ΔP_s

Point	Clock Time	Dry Gas Meter, CF	"Pitot" "H ₂ O	Orifice ΔH "H ₂ O Desired	Orifice ΔH "H ₂ O Actual	Pump Vacuum "Hg Gauge	Stack Temp °F	Probe Temp °F	Oven Temp °F	Effluent Temp °F	Dry Gas Temp °F Inlet	Dry Gas Temp °F Outlet	T _m	Remarks
1	1500	274.902	0.52	1.10	5.5	148	327	328	54	87	87	87		
5	1502.5	276.41	0.50	1.05	5.5	148	326	327	60	87	87	87		
4	1505	277.60	0.48	1.00	5.0	148	324	327	62	87	87	87		
3	1507.5	279.00	0.42	0.88	5.0	148	327	327	62	87	87	87		
2	1510	280.62	0.36	0.76	4.5	148	328	328	61	87	88	88		
1	1512.5	281.71	0.33	0.69	4.5	148	328	329	62	88	88	88		
End	1515	282.826	-	-	-	-	-	-	-	-	-	-		
6	1532	282.826	0.48	1.00	5.5	148	325	325	325	327	86	86		
5	1534.5	284.49	0.50	1.05	5.8	148	328	327	327	328	86	86		
4	1537	285.63	0.50	1.05	5.5	148	327	327	61	86	86	86		
3	1539.5	287.15	0.46	0.97	0.97	148	328	327	62	86	86	86		
2	1542	288.52	0.36	0.76	4.5	148	327	327	60	87	88	88		
1	1544.5	289.47	0.28	0.59	4.0	148	326	325	60	88	87	87		
End	1547	290.788	-	-	-	-	-	-	-	-	-	-		
3	1555	290.788	0.47	0.99	6.0	148	328	327	61	88	87	87		
5	1557.5	292.04	0.44	0.93	5.5	148	326	327	61	88	86	86		
4	1560	293.37	0.41	0.86	5.3	148	327	328	60	88	87	87		
3	1562.5	294.77	0.38	0.80	5.0	149	324	327	57	88	87	87		

Pitot Tube Calibration Factor C_p 0.320 ✓
 Volume Collected V_m 31.404 31.2716 ft³ ✓
 Water Collected V_w 201.2 ml ✓
 Time of Test T_t 60 min. ✓
 Stack Pressure P_s -0.34 "H₂O ✓

Barometer No. T4-E5C-8 ✓
 Total Volume of Leak Checks After Start: — ft³ ✓
 Probe Tip Dia. D_n 0.256 in. ✓
 % CO₂ 14.5 ✓ % CO 0.0 ✓
 % O₂ 3.7 ✓ % N₂ 81.8 ✓
 Area Stack A_s 22.167 in² ✓

Pitot Tube No. T4-E5C-8 ✓
 Baro. Press. P_b 2.42 "Hg ✓
 Probe Tip Dia. D_n 0.256 in. ✓
 % CO₂ 14.5 ✓ % CO 0.0 ✓
 % O₂ 3.7 ✓ % N₂ 81.8 ✓
 Area Stack A_s 22.167 in² ✓

Barometer No. 49-2 ✓
 Total Volume of Leak Checks After Start: — ft³ ✓
 V_m = Dry Gas Meter Calibration Factor 1.039 ✓ X 31.276 ✓
 1.000 ✓
 {Dry Gas Meter Reading — ft³ - (T_t — min. X Leak Rate — cfm)}

Impinger Box No. BR1

			<u>Water Weight Gain</u>		
Impinger 1	Final Weight	<u>798.7</u>		Impinger 1	<u>192.7</u>
	Initial Weight	<u>606.0</u>			
	Increase			Impinger 2	<u>110</u>
Impinger 2	Final Weight	<u>560.6</u>		Impinger 3	<u>-2.4</u>
	Initial Weight	<u>559.5</u>		Impinger 4	<u>9.8</u>
	Increase			Impinger 5	
Impinger 3	Final Weight	<u>725.2</u>	$V_w =$	Impinger 5	
	Initial Weight	<u>727.6</u>	$g SO_2 =$		
	Increase		$V_w =$	Impinger 6	
Impinger 4	Final Weight	<u>988.3</u>		Impinger 7	
	Initial Weight	<u>978.5</u>		Total	<u>201.2 ✓ = Vw</u>
	Increase				
Impinger 5	Final Weight		$P_b = \frac{29.92}{31.40} \checkmark$	%CO ₂ =	<u>14.5 ✓</u>
	Initial Weight		$V_m = \frac{31.276}{31.40} \checkmark$	%O ₂ =	<u>3.7 ✓</u>
	Increase		$V_w = \frac{20.1.2}{31.40} \checkmark$	%CO =	<u>80 ✓</u>
Impinger 6	Final Weight		$P_m = \frac{0.892}{0.423} \checkmark$	%N ₂ =	<u>81.8 ✓</u>
	Initial Weight		Avg ΔP = $\frac{0.4225}{0.423} \checkmark$	A _s =	<u>22167 ✓</u>
	Increase			D _n =	<u>0.250 ✓</u>
Impinger 7	Final Weight		Avg $\sqrt{\Delta P} = \frac{0.647}{0.423} \checkmark$	T _t =	<u>60 ✓</u>
	Initial Weight		C _p = <u>0.820 ✓</u>		
	Increase		P _s = <u>-0.74 H₂O ✓</u>	29.90 ✓	"Hg
			T _m = <u>87 °F</u>	547 ✓	°R
			T _s = <u>149 °F</u>	609 ✓	°R
<u>Moisture Content:</u>			<u>23.89 ✓</u>	<u>0.7611 ✓</u>	
	%M = <u>23.82 TF</u>	M _d = <u>0.7618 TF</u>	MW _d = <u>30.465 ✓</u>	MW = <u>27.50 27.49 ✓</u>	

$$Vm_{std} = 17.65 \quad Vm \left[\frac{P_b + \frac{P_m}{13.6}}{T_m + 460} \right] = 17.65 \times \frac{31.276}{31.40} \left[\frac{29.92 + \frac{0.892}{13.6}}{87 + 460} \right] = \frac{30.261}{\frac{0.566}{0.504} scfm} \checkmark$$

$$Vw_{gas} = 0.0472 \times Vw = 0.0472 \times \frac{201.2}{23.89} = \frac{9.497}{23.89} \checkmark \text{ sft}^3$$

$$\% \text{ Moisture} = \frac{Vw_{gas}}{Vm_{std} + Vw_{gas}} \times 100 = \frac{9.497}{30.261 \frac{23.82 TF}{23.82 TF} + 9.497} \times 100 = \frac{23.82 TF}{23.82 TF} \% \checkmark$$

$$V_s = 5123.8 \times \frac{0.647}{27.50 \times 29.90} \times \frac{2340}{2340} \checkmark \times \frac{0.820}{0.820} = \frac{2334}{2334} \text{ fpm}$$

$$\%I = \frac{1.039 \times \frac{30.261}{30.384 TF} \times \frac{60}{60} \times \frac{2334}{2334} \times \frac{29.90}{29.90} \times (0.250)^2}{18.7618 \times 60 \times 2340} = \frac{95.9}{96.2} \checkmark \%$$

$$ACFM: \frac{360.197}{260.192 TF} \checkmark$$

$$SCFM: \frac{238.409}{238.527 TF} \checkmark$$

$$\%EA: \frac{20.4}{20.4} \checkmark$$

5010 Thru 28 FIELD DATA

3
West FCCV
7/11/10

Run Number

Unit

Date

Point	Clock Time	Dry Gas Meter, CF	"Pitot" "H ₂ O	Orifice ΔH "H ₂ O Desired	Orifice ΔH "H ₂ O Actual	Pump Vacuum "Hg Gauge	Stack Temp °F	Probe Temp °F	Oven Temp °F	Effluent Temp °F	Dry Gas Temp °F Inlet	Dry Gas Temp °F Outlet	Remarks
2	1605	2466.61	0.30	0.63	0.63	5.5	150	323	330	62	67	86	
1	1607.5	247.29	0.30	0.63	0.63	5.0	150	321	324	62	87	87	
END	1610	248.245	-	-	-	-	-	-	-	-	-	-	
A	1621	298.245	0.55	1.20	1.20	7.5	151	328	328	61	88	85	
5	1623.5	299.58	0.55	1.20	1.20	7.5	151	324	325	61	88	88	
4	1626	300.53	0.46	0.97	0.97	7.0	152	324	326	61	89	88	
3	1628.5	302.11	0.41	0.86	0.86	8.5	151	326	326	60	88	88	
2	1631	303.60	0.38	0.80	0.80	7.0	152	323	324	61	87	87	
1	1633.5	304.69	0.30	0.63	0.63	7.0	152	324	324	60	88	87	
END	1636	306.178	-	-	-	-	-	-	-	-	-	-	

PRELIMINARY VELOCITY TRAVERSE DATA
AND
SAMPLING LOCATION DATA

Job Number 10-274Job Name Citgo

Stack Height _____ ft.

Sampling Location FCCU

Sampling Port Height Above Ground _____ ft.

Date 6/20/10 Time 1930

	<u>Port A</u>	<u>Port B</u>	<u>Port C</u>	<u>Port D</u>	<u>Average</u>
Port & Inside Diameter (in.)	_____	_____	_____	_____	_____
Port & Wall Thickness (in.)	_____	_____	_____	_____	_____
Inside Stack Diameter (in.)	_____	_____	_____	_____	_____

Sampling Ports are _____ ft. _____ in. (_____ stack diameters) downstream from disturbance (inlet, constriction, bend, expansion)

Sampling Ports are _____ ft. _____ in. (_____ stack diameters) upstream from disturbance (outlet, constriction, bend, expansion)

Point Number	Percent Diameter	Distance from Ref. Point (decimal in.)	Distance from Ref. Point (fractional in.)	Port A $\Delta P/T_s/\alpha$	Port B $\Delta P/T_s/\alpha$	Port C $\Delta P/T_s/\alpha$	Port D $\Delta P/T_s/\alpha$
1	—	—	—	-1-1-	-1-1-	-1-1-	-1-1-
2				0.30114915	0.29114915	0.27114910	0.31115110
3				0.33114910	0.31114910	0.37114915	0.32115010
4				0.40115010	0.39114910	0.38114910	0.39114915
5				0.5111511-10	0.5011491-10	0.50114910	0.46114910
6				0.5411501-10	0.54114910	0.5411491-5	0.48114910
7				0.56114910	0.55114910	0.53114910	0.4511491-5
8				/ /	/ /	/ /	/ /
9				/ /	/ /	/ /	/ /
10				/ /	/ /	/ /	/ /
11				/ /	/ /	/ /	/ /
12				/ /	/ /	/ /	/ /
13				/ /	/ /	/ /	/ /
14				/ /	/ /	/ /	/ /
15				/ /	/ /	/ /	/ /
16				/ /	/ /	/ /	/ /
17				/ /	/ /	/ /	/ /
18				/ /	/ /	/ /	/ /
19				/ /	/ /	/ /	/ /
20				/ /	/ /	/ /	/ /
21				/ /	/ /	/ /	/ /
22				/ /	/ /	/ /	/ /
23				/ /	/ /	/ /	/ /
24				/ /	/ /	/ /	/ /

Pitot Tube No. T4-E-8Average ΔP 0.428 $C_p = 6.820$ Average $\Delta P^{1/2}$ 0.150 $P_b = 25.54$ "HgAverage T_s 150 °F $P_a = 0.32$ "H₂OAverage α 0.833 degrees $A_s = 22167$ in.²

25



APPENDIX E

Analytical Data

METCO Environmental

Particulate Analysis Summary

Job Number 10-274
 Job Name CIT 68
 Location Lemont, IL

Date Analysis Completed 7/16/10
 Unit Tested FCCU WESP Stack

Run No.	1	2	3		
Particulate on Filter (mg)	74.2	68.2	27.1	28.1 μ m	08/10/10
Particulate in Front Wash (mg)*	18.3	0.0	12.0		
MF (mg)	92.5	68.2	39.1	40.1 μ	
Particulate in Impinger #1 (mg)**					
MT (mg)					

REI

Analyst

* Less Acetone Residue

** Less Ammonium Sulfate

METCO Environmental
Particulate Analysis EPA Method 5 131202

Job Number 10-274
Job Name CITGO

Stack Filters

Location Lemont, IL
Unit Tested KCCUWES PStack

Desiccator Time In	1500	7/14	1620	7/13	1625	7/14		
Desiccator Time Out	1615	7/15	1620	7/14	1630	7/15		

Run No.	<u>1</u>	Filter No.	<u>G88W104</u>					
Filter & Particulate + Tare Weight (g)								
Tare Weight (g)								
Filter & Particulate (g)	<u>0.4987</u>	<u>0.4986</u>	x					

Filter & Particulate Average (g) 0.4986
Initial Filter Weight (g) 0.4224

Total Particulate (mg) 74.2

Run No.	<u>2</u>	Filter No.	<u>G88W107</u>	<u>G88W105</u>				
Filter & Particulate + Tare Weight (g)								
Tare Weight (g)								
Filter & Particulate (g)	<u>0.4491</u>	<u>0.4884</u>	<u>0.4888</u>					

Filter & Particulate Average (g) 0.4888
Initial Filter Weight (g) 0.4206

Total Particulate (mg) 68.2

Run No.	<u>3</u>	Filter No.	<u>G88W107</u>					
Filter & Particulate + Tare Weight (g)								
Tare Weight (g)								
Filter & Particulate (g)	<u>0.4491</u>	<u>0.4513</u>	<u>0.4517</u>					

Filter & Particulate Average (g) 0.4517
Initial Filter Weight (g) 0.4236

Total Particulate (mg) 27.1

Run No.	<u>1314</u>	Filter No.	<u>G88Y99</u>					
Filter & Particulate + Tare Weight (g)								
Tare Weight (g)								
Filter & Particulate (g)	<u>0.4011</u>	<u>0.4010</u>	x					

Mettler AE240

Filter & Particulate Average (g) 0.4010
Initial Filter Weight (g) 0.4003

Total Particulate (mg) 0.71

REK

Analyst

METCO Environmental
Particulate Analysis EPA Method 5 *B1202*

Front Wash

Job Number 10-274
Job Name CITGO

Location Lemon, IL
Unit Tested FCC WESP Stark

Desiccator Time In	1500	7/12	1600	7/13	1645	7/14		
Desiccator Time Out	1518	7/13	1600	7/14	0945	7/16		

Run No.	<u>1</u>	Volume (ml)	<u>1.98</u>					
Final Weight (g)	<u>167.7143</u>	<u>167.7136</u>	<u>167.7133</u>					
Initial Weight (g)	<u>167.6946</u>	<u>167.6946</u>	<u>167.6946</u>					
Particulate Weight (g)	<u>0.0197</u>	<u>0.0190</u>	<u>0.0187</u>					

Particulate Average (mg) 18.7
Less Acetone Blank (mg) 0.4
Total Particulate (mg) 18.3

Run No.	<u>2</u>	Volume (ml)	<u>80</u>					
Final Weight (g)	<u>168.4437</u>	<u>168.4428</u>	<u>168.4424</u>					
Initial Weight (g)	<u>168.4424</u>	<u>168.4424</u>	<u>168.4424</u>					
Particulate Weight (g)	<u>0.0013</u>	<u>0.0004</u>	<u>0.0000</u>					

Particulate Average (mg) 0.0
Less Acetone Blank (mg) 0.2
Total Particulate (mg) 0.0

Run No.	<u>3</u>	Volume (ml)	<u>155</u>					
Final Weight (g)	<u>136.0276</u>	<u>136.0265</u>	<u>136.0266</u>					
Initial Weight (g)	<u>136.0143</u>	<u>136.0143</u>	<u>136.0143</u>					
Particulate Weight (g)	<u>0.0133</u>	<u>0.0122</u>	<u>0.0123</u>					

Particulate Average (mg) 12.3
Less Acetone Blank (mg) 0.3
Total Particulate (mg) 12.0

Acetone Blank	Volume (ml)	<u>137</u>						
Final Weight (g)	<u>177.2138</u>	<u>177.2135</u>						
Initial Weight (g)	<u>177.2132</u>	<u>177.2132</u>						
Difference (g)	<u>0.0006</u>	<u>0.0003</u>						

Mettler AE240.00

Average (mg) 0.3
* mg/l 2.2

* Note: If greater than 7.9 mg/l, use 7.9 mg/l.

PEA

Analyst

METCO Environmental

Particulate Analysis Summary

Job Number 10-274Date Analysis Completed Lemont, ILJob Name CITCOUnit Tested FCCU WESP Stack

Location _____

✓ ✓ ✓

Run No.	1	2	3		
Particulate on Filter (mg)	93.9	84.3	33.1		
Particulate in Front Wash (mg)*	11.3	3.3	4.2		
MF (mg)	105.2	87.6	37.3		
Particulate in Impinger #1 (mg)**					
MT (mg)					

REA

Analyst

* Less Acetone Residue

** Less Ammonium Sulfate

METCO Environmental
Particulate Analysis EPA Method 5 13/28

Stack Filters

Job Number 10-274
Job Name CITGO

Location Lemont IL
Unit Tested FCC UWESP Stack 6

Desiccator Time In	1500	7/12	1625	7/13	1630	7/14		
Desiccator Time Out	1620	7/13	1625	7/14	1635	7/15		

Run No.	<u>1</u>	Filter No.	<u>G88W101</u>					
Filter & Particulate + Tare Weight (g)								
Tare Weight (g)								
Filter & Particulate (g)	<u>0.5271</u>	<u>0.5178</u>	<u>0.5182</u>					

Filter & Particulate Average (g) 0.5182
Initial Filter Weight (g) 0.4243

Total Particulate (mg) 89.39

Run No.	<u>2</u>	Filter No.	<u>G88W106</u>					
Filter & Particulate + Tare Weight (g)								
Tare Weight (g)								
Filter & Particulate (g)	<u>0.5048</u>	<u>0.5000</u>	<u>0.5004</u>					

Filter & Particulate Average (g) 0.5004
Initial Filter Weight (g) 0.4214

Total Particulate (mg) 84.3

Run No.	<u>3</u>	Filter No.	<u>G88W108</u>					
Filter & Particulate + Tare Weight (g)								
Tare Weight (g)								
Filter & Particulate (g)	<u>0.4560</u>	<u>0.4558</u>	<u>/</u>					

Filter & Particulate Average (g) 0.4558
Initial Filter Weight (g) 0.4242

Total Particulate (mg) 33.1

Run No.	<u>P/K</u>	Filter No.	<u>G88W100</u>					
Filter & Particulate + Tare Weight (g)								
Tare Weight (g)								
Filter & Particulate (g)	<u>0.3956</u>	<u>0.3957</u>	<u>/</u>					

Mettler AE240

Filter & Particulate Average (g) 0.3957
Initial Filter Weight (g) 0.3951

Total Particulate (mg) 0.6

REA

Analyst

METCO Environmental
Particulate Analysis EPA Method 5B/OTM128

Front Wash

Job Number 10-274
Job Name C1760

Location Hennont, IL
Unit Tested FCC 4 W ESP Stack

Desiccator Time In	1500	7/12	1615	7/13			
Desiccator Time Out	1530	7/13	1615	7/14			

Run No.	<u>1</u>	Volume (ml)	<u>212</u>				
Final Weight (g)	<u>134.3304</u>	<u>134.3306</u>					
Initial Weight (g)	<u>134.3193</u>	<u>134.3193</u>					
Particulate Weight (g)	<u>0.0111</u>	<u>0.0113</u>	✓				

Particulate Average (mg) 11.3
Less Acetone Blank (mg) 0
Total Particulate (mg) 11.3 ✓

Run No.	<u>2</u>	Volume (ml)	<u>63</u>				
Final Weight (g)	<u>139.7534</u>	<u>139.7534</u>					
Initial Weight (g)	<u>139.7501</u>	<u>139.7501</u>					
Particulate Weight (g)	<u>0.0833</u>	<u>0.0033</u>	✓				

Particulate Average (mg) 3.3
Less Acetone Blank (mg) 0
Total Particulate (mg) 3.3 ✓

Run No.	<u>3</u>	Volume (ml)	<u>148</u>				
Final Weight (g)	<u>155.2613</u>	<u>155.2613</u>					
Initial Weight (g)	<u>155.2571</u>	<u>155.2571</u>					
Particulate Weight (g)	<u>0.0042</u>	<u>0.0042</u>	✓				

Particulate Average (mg) 4.2
Less Acetone Blank (mg) 0
Total Particulate (mg) 4.2 ✓

Acetone Blank	Volume (ml)	<u>147</u>					
Final Weight (g)	<u>165.7879</u>	<u>165.7880</u>					
Initial Weight (g)	<u>165.7880</u>	<u>165.7880</u>					
Difference (g)		<u>0</u>	<u>0</u>				

Mettler AE240 00 Average (mg) 0
* mg/l _____

* Note: If greater than 7.9 mg/l, use 7.9 mg/l.

REA

Analyst

Initial Stack Filter Weights

Glass
Fiber88mm M Series

Dessicator

Analyst M.L.

IN Date/Time	1/31/09 #1-121	1	2/6/09 1/121-132	1
OUT Date/Time	1	1	1	1

1	0.4245	0.4245	0.	45	0.4262	0.4262	0.	89	0.4234	0.4233	0.
2	0.4249	0.4249	0.	46	0.4240	0.4240	0.	90	0.4174	0.4176	0.
3	0.4204	0.4203	0.	47	0.4257	0.4258	0.	91	0.4263	0.4262	0.
4	0.4215	0.4214	0.	48	0.4239	0.4236	0.	92	0.4235	0.4232	0.
5	0.4273	0.4273	0.	49	0.4227	0.4227	0.	93	0.4227	0.4227	0.
6	0.4198	0.4197	0.	50	0.4227	0.4227	0.	94	0.4159	0.4160	0.
7	0.4226	0.4224	0.	51	0.4193	0.4192	0.	95	0.4253	0.4253	0.
8	0.4239	0.4240	0.	52	0.4246	0.4247	0.	96	0.4178	0.4197	0.
9	0.4209	0.4207	0.	53	0.4221	0.4221	0.	97	0.4250	0.4249	0.
10	0.4215	0.4215	0.	54	0.4195	0.4194	0.	98	0.4243	0.4243	0.
11	0.4265	0.4265	0.	55	0.4263	0.4263	0.	99	0.4253	0.4253	0.
12	0.4239	0.4237	0.	56	0.4219	0.4219	0.	100	0.4170	0.4190	0.
13	0.4250	0.4249	0.	57	0.4205	0.4204	0.	101	0.4243	0.4243	0.
14	0.4293	0.4293	0.	58	0.4284	0.4284	0.	102	0.4230	0.4231	0.
15	0.4265	0.4264	0.	59	0.4207	0.4207	0.	103	0.4234	0.4238	0.
16	0.4195	0.4195	0.	60	0.4209	0.4208	0.	104	0.4226	0.4224	0.
17	0.4239	0.4238	0.	61	0.4186	0.4184	0.	105	0.4207	0.4206	0.
18	0.4281	0.4280	0.	62	0.4212	0.4210	0.	106	0.4163	0.4161	0.
19	0.4254	0.4254	0.	63	0.4254	0.4254	0.	107	0.4238	0.4236	0.
20	0.4203	0.4202	0.	64	0.4229	0.4227	0.	108	0.4229	0.4227	0.
21	0.4214	0.4213	0.	65	0.4219	0.4218	0.	109	0.4215	0.4213	0.
22	0.4220	0.4219	0.	66	0.4189	0.4187	0.	110	0.4199	0.4199	0.
23	0.4284	0.4283	0.	67	0.4205	0.4203	0.	111	0.4196	0.4196	0.
24	0.4219	0.4217	0.	68	0.4198	0.4197	0.	112	0.4211	0.4211	0.
25	0.4211	0.4211	0.	69	0.4207	0.4206	0.	113	0.4215	0.4214	0.
26	0.4236	0.4237	0.	70	0.4164	0.4163	0.	114	0.4194	0.4193	0.
27	0.4294	0.4294	0.	71	0.4136	0.4136	0.	115	0.4193	0.4193	0.
28	0.4235	0.4236	0.	72	0.4179	0.4177	0.	116	0.4191	0.4191	0.
29	0.4272	0.4273	0.	73	0.4221	0.4217	0.	117	0.4226	0.4226	0.
30	0.4282	0.4282	0.	74	0.4230	0.4229	0.	118	0.4214	0.4213	0.
31	0.4211	0.4211	0.	75	0.4225	0.4226	0.	119	0.4216	0.4216	0.
32	0.4238	0.4238	0.	76	0.4189	0.4189	0.	120	0.4232	0.4231	0.
33	0.4266	0.4266	0.	77	0.4172	0.4172	0.	121	0.4196	0.4196	0.
34	0.4218	0.4217	0.	78	0.4237	0.4236	0.	122	0.4153	0.4152	0.
35	0.4268	0.4268	0.	79	0.4237	0.4237	0.	123	0.4443	0.4442	0.
36	0.4260	0.4259	0.	80	0.4228	0.4226	0.	124	0.4419	0.4418	0.
37	0.4231	0.4229	0.	81	0.4188	0.4186	0.	125	0.4445	0.4444	0.
38	0.4292	0.4290	0.	82	0.4179	0.4178	0.	126	0.4454	0.4453	0.
39	0.4259	0.4258	0.	83	0.4230	0.4230	0.	127	0.4272	0.4271	0.
40	0.4196	0.4195	0.	84	0.4233	0.4231	0.	128	0.4306	0.4306	0.
41	0.4279	0.4279	0.	85	0.4227	0.4226	0.	129	0.4273	0.4273	0.
42	0.4238	0.4238	0.	86	0.4142	0.4142	0.	130	0.4239	0.4228	0.
43	0.4283	0.4283	0.	87	0.4243	0.4243	0.	131	0.4254	0.4253	0.
44	0.4235	0.4235	0.	88	0.4233	0.4233	0.	132	0.4237	0.4237	0.
OUT 1 1/31/09	OUT 2 2/1/09	OUT 2 2/3/09	OUT 2 2/3/09	OUT 1 2/1/09	OUT 1 2/3/09	OUT 2 2/3/09	OUT 2 2/3/09	OUT 2 2/3/09	OUT 1 2/1/09	OUT 1 2/3/09	OUT 2 2/3/09

Initial Stack Filter Weights

G 88mm Y Series
DessicatorAnalyst YMB

IN Date/ Time	1/12/10 1	/	/	/
OUT Date/ Time	/	/	/	/

1	0.4204	0.4203	0.	45	0.4233	0.4232	0.	89	0.4211	0.4210	0.
2	0.4223	0.4222	0.	46	0.4221	0.4221	0.	90	0.4017	0.4016	0.
3	0.4217	0.4216	0.	47	0.4239	0.4239	0.	91	0.3931	0.3931	0.
4	0.4242	0.4242	0.	48	0.4169	0.4168	0.	92	0.3962	0.3961	0.
5	0.4257	0.4256	0.	49	0.4229	0.4228	0.10-16	93	0.3977	0.3977	0.
6	0.4237	0.4238	0.	50	0.4180	0.4180	0.	94	0.3937	0.3937	0.
7	0.4217	0.4216	0.	51	0.4272	0.4272	0.	95	0.3934	0.3935	0.
8	0.4271	0.4270	0.	52	0.4154	0.4154	0.16-16	96	0.4000	0.4000	0.
9	0.4250	0.4250	0.	53	0.4229	0.4229	0.10-16	97	0.3959	0.3962	0.
10	0.4229	0.4229	0.	54	0.4184	0.4184	0. "	98	0.3969	0.3969	0.
11	0.4205	0.4205	0.	55	0.4123	0.4123	0. "	99	0.4003	0.4003	0.
12	0.4223	0.4221	0.	56	0.4243	0.4243	0. "	100	0.3951	0.3951	0.
13	0.4217	0.4217	0.	57	0.4197	0.4197	0. "	101	0.3973	0.3972	0.
14	0.4248	0.4247	0.	58	0.4155	0.4155	0.	102	0.3955	0.3954	0.
15	0.4002	0.4002	0.	59	0.4253	0.4253	0.10-16	103	0.3979	0.3979	0.
16	0.4120	0.4120	0.	60	0.4221	0.4227	0.	104	0.3974	0.3973	0.
17	0.4145	0.4146	0.	61	0.4176	0.4176	0.	105	0.3908	0.3908	0.
18	0.4166	0.4166	0.	62	0.4144	0.4144	0.	106	0.3968	0.3967	0.
19	0.4178	0.4176	0.	63	0.4211	0.4211	0.	107	0.3966	0.3966	0.
20	0.4147	0.4147	0.	64	0.4228	0.4228	0.	108	0.3963	0.3962	0.
21	0.4184	0.4183	0.	65	0.4149	0.4148	0.	109	0.3922	0.3922	0.
22	0.4112	0.4113	0.	66	0.4237	0.4236	0.	110	0.3990	0.3990	0.
23	0.3930	0.3931	0.	67	0.4181	0.4181	0.	111	0.3993	0.3993	0.
24	0.3946	0.3946	0.	68	0.4118	0.4118	0.	112	0.3967	0.3967	0.
25	0.4174	0.4174	0.10-176	69	0.4242	0.4241	0.	113	0.3930	0.3930	0.
26	0.4192	0.4193	0. "	70	0.4220	0.4219	0.	114	0.3980	0.3980	0.
27	0.3910	0.3910	0. "	71	0.4157	0.4156	0.	115	0.4014	0.4013	0.
28	0.4170	0.4170	0. "	72	0.4148	0.4147	0.	116	0.3935	0.3935	0.
29	0.4198	0.4197	0.10-176	73	0.4230	0.4230	0.10-54	117	0.3963	0.3964	0.
30	0.3924	0.3924	0. "	74	0.4232	0.4232	0.5	118	0.4001	0.4001	0.
31	0.4166	0.4167	0. "	75	0.4173	0.4173	0.5	119	0.3950	0.3950	0.
32	0.4173	0.4174	0. "	76	0.4249	0.4249	0.1	120	0.3947	0.3946	0.
33	0.3905	0.3903	0.10-139	77	0.4250	0.4249	0.10-54	121	0.3979	0.3980	0.10-141
34	0.3981	0.3981	0. "	78	0.4159	0.4160	0.5	122	0.3937	0.3938	0. "
35	0.3988	0.3989	0. "	79	0.4239	0.4240	0. }	123	0.3979	0.3980	0.
36	0.3918	0.3918	0. "	80	0.4254	0.4253	0. }	124	0.3944	0.3945	0.
37	0.4222	0.4221	0.	81	0.4201	0.4201	0.	125	0.3943	0.3943	0.
38	0.4187	0.4187	0.	82	0.4176	0.4176	0.	126	0.4010	0.4011	0.10-253
39	0.4238	0.4239	0.	83	0.4231	0.4230	0.	127	0.3952	0.3952	0.
40	0.4200	0.4200	0.	84	0.4171	0.4171	0.	128	0.3969	0.3969	0.
41	0.4174	0.4174	0.	85	0.4148	0.4147	0.	129	0.3912	0.3912	0.
42	0.4219	0.4219	0.	86	0.4231	0.4231	0.	130	0.3978	0.3977	0.
43	0.4205	0.4204	0.	87	0.4136	0.4136	0.	131	0.3944	0.3944	0.
44	0.4195	0.4194	0.	88	0.4167	0.4168	0.	132	0.3968	0.3968	0.

LABORATORY QUALITY ASSURANCE DATA

BALANCE ID Mettler AE 240
S/N K 51852

Weights 09180701

DATE & TIME		100g STD	1.0g STD	0.5g STD	ANALYST	REMARKS
7/11/08	Actual (g)	100,0000	1,0001	0,5000	REA	
0930	Difference (mg)	0	+0,1	0		
100	Actual (g)	100,0000	1,0000	0,5000	REA	
7/15	Difference (mg)	0	0	0		
0945	Actual (g)	100,0000	1,0000	0,5000	REA	
7/16	Difference (mg)	0	0	0		
0900	Actual (g)	99,9999	1,0001	0,5000	REA	
7/14	Difference (mg)	-0,1	+0,1	0		
0900	Actual (g)	100,0001	1,0001	0,5000	REA	
7/20/08	Difference (mg)	+0,1	+0,1	0		
0830	Actual (g)	100,0000	1,0000	0,5000	REA	
7/24/08	Difference (mg)	0	0	0		
0830	Actual (g)	99,9999	1,0000	0,5000	REA	
7/24/08	Difference (mg)	-0,1	0	0		
	Actual (g)		.			
	Difference (mg)					
	Actual (g)					
	Difference (mg)					
	Actual (g)					
	Difference (mg)					
	Actual (g)					
	Difference (mg)					



LABORATORY QUALITY ASSURANCE DATA

BALANCE ID Mettler AE200SN 37636

Weights 0918079

DATE & TIME		100g STD	1.0g STD	0.5g STD	ANALYST	REMARKS
0930	Actual (g)	99,9999	1,0001	0,5000	REA	
7/9/10	Difference (mg)	-0,1	+0,1	0		
1100	Actual (g)	100,0001	1,0001	0,5001	REA	
7/13/10	Difference (mg)	+0,1	+0,1	+0,1		
0825	Actual (g)	100,0001	1,0000	0,5000	REA	
7/13/10	Difference (mg)	+0,1	0	0		
0930	Actual (g)	100,0000	1,0000	0,5000	REA	
7/14/10	Difference (mg)	0	0	0		
1100	Actual (g)	100,0000	1,0001	0,5000	REA	
7/13/10	Difference (mg)	0	+0,1	0		
0945	Actual (g)	99,9999	1,0000	0,5000	REA	
7/16/10	Difference (mg)	-0,1	0	0		
0900	Actual (g)	99,9999	1,0000	0,5000	REA	
7/12/10	Difference (mg)	-0,1	0	0		
1330	Actual (g)	99,9999	0,9999	0,4999	REA	
7/21/10	Difference (mg)	-0,1	-0,1	-0,1		
0830	Actual (g)	100,0000	10001	0,5000	REA	
7/22/10	Difference (mg)	0	+0,1	0		
	Actual (g)					
	Difference (mg)					
	Actual (g)					
	Difference (mg)					
	Actual (g)					
	Difference (mg)					



APPENDIX F

Plant Operational Data

Shapley, Ned

From: Romans, Trevor
Sent: Thursday, August 05, 2010 4:43 PM
To: Shapley, Ned
Subject: FW: Coke Burn Rates

From: Hutcherson, Mike
Sent: Thursday, August 05, 2010 4:11 PM
To: Romans, Trevor
Subject: FW: Coke Burn Rates

CITGO Coke burn rates

Mike Hutcherson
Director of Field Operations
METCO Environmental
972-931-7127 phone
972-931-8398 fax
www.metcoenv.com

From: Case, Paul [mailto:pcase@citgo.com]
Sent: Thursday, August 05, 2010 4:09 PM
To: Hutcherson, Mike
Cc: Cordina, Matt; Klickman, Matt; Case, Paul
Subject: Coke Burn Rates

Mike, here are the coke burn rates for the time period specified

Run	Start	End	coke burn rate (lb/hr)
1	6/30/2010 19:08	6/30/2010 20:34	61,869.6
2	7/1/2010 12:08	7/1/2010 13:46	61,222.4
3	7/1/2010 15:00	7/1/2010 16:36	60,881.3

Paul Case
FCC Unit Operations Process Engineer
630-257-4359



APPENDIX G

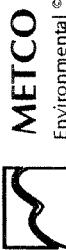
Chain of Custody



CHAIN OF CUSTODY RECORD

				Project Manager: <u>M. Huthersen</u>		Project Supervisor: <u>T. Cutts</u>		Method: <u>SB/202</u>			
SAMPLE I.D.	DATE	TIME	Absorb. Solution	Initial Vol.	P	A	H	C	S	O	Recovered by
#	O	F	C	N	R	L	C	L	O	S	J Cutts
Run 1 Filter	6/30/10	2150	1	DI							
Run 1 FH		2152	1								
Run 1 Imp Wash		2153	1								
Run 2 Filter	7/1/10	1525	1								
Run 2 FH		1430	1								
Run 2 BH Imp 1-3		1535	1	DI							
Run 2 Imp Wash		1540	1								
Run 3 Filter		1810	1								
Run 3 FH		1815	1								
Run 3 BH Imp 1-3		1820	1	DI							
Run 3 Imp Wash		1825	1								

Samples Received for Transport/Shipment by: James Bryant Date: 7/21/10 Time: 1500
 Samples Received for Transport/Shipment by: _____ Date: _____ Time: _____
 Samples Received for Transport/Shipment by: _____ Date: _____ Time: _____
 Samples Shipped Via: _____ Date: _____ Time: _____
 Samples Received at Laboratory by: Daryl Cutts Date: 7/21/10 Time: 0740
 Samples Analyzed by: John Allen Date: 7/21/10 Time: 0945
 Samples Analyzed by: _____ Date: _____ Time: _____
 Data Checked by: J Cutts Date: 08/10/10 Time: 1200



CHAIN OF CUSTODY RECORD

Page 2 of 2

Job No.: <u>10-274</u> Job Name: <u>Citgo</u> Location: <u>Lemont, IL</u> Unit: <u>FCCU WSGP Stack</u>				Project Manager: <u>Hutcherson</u> Project Supervisor: <u>Cutler</u> Method: <u>SBC / 202</u>									
				SAMPLE ANALYSIS REQUIRED				REMARKS <small>(Specific Compounds/Methods)</small>					
SAMPLE I.D.	DATE	TIME	#	Absorb. Solution	Initial Vol.	P	A	H	C	L	O	S	RECOVERED by
						O	F	C	N	T	L	T	T
Blank Pi	7/10/00	1310			1								J Cutler
Blank Acetone		1315			1								
Blank Filter		1316			1								
Blank Methylene		1317			1								
Samples Received for Transport/Shipment by: <u>Doreen Brumley</u> Samples Received for Transport/Shipment by: _____ Samples Received for Transport/Shipment by: _____ Samples Shipped Via: _____ Samples Received at Laboratory by: <u>Doreen Brumley</u> Samples Analyzed by: <u>Doreen Brumley</u> Samples Analyzed by: _____ Data Checked by: <u>✓</u>													Date: <u>7/21/00</u> Time: <u>1500</u> Date: _____ Time: _____ Date: _____ Time: _____ Date: _____ Time: _____ Date: <u>7/21/00</u> Time: <u>0945</u> Date: <u>7/16/00</u> Time: <u>0945</u> Date: <u>08/10/00</u> Time: <u>1220</u>



CHAIN OF CUSTODY RECORD

Page 1 of 2

Job No.:	10-274	Project Manager:	M. Hutcherson	Method:	5B/ DTM 28
Job Name:	Citgo	Project Supervisor:	J. Cutrone		
Location:	Lemoat, IL				
Unit:	Wasp ECU				
SAMPLE I.D.	DATE	TIME	Absorb. Solution	Initial Vol.	SAMPLE ANALYSIS REQUIRED
#	O F	C O N T	T	P A R T	Recovered by
Run 1 PM Filter	6/30/0	2155	-	H C L 2	REMARKS (Specific Compounds/Methods)
Run 1 FH		2152	-	S O 2	
Run 1 BH imp 1-2		2157	-		
Run 1 Methylenic wash		2157	-		
Run 1 CPM Filter		2157	-		
Run 2 PM Filter	7/1/0	1400	-		
Run 2 FH		1405	-		
Run 2 BH imp 1-2		1525	-		
Run 2 methylenic wash		1530	-		
Run 2 CPM Filter		1535	-		
Run 3 PM Filter		1810	-		
Run 3 FH		1615	-		
Run 3 BH imp 1-2		1815	-		
Run 3 Methylenic wash		1820	-		
Samples Received for Transport/Shipment by:	<u>Brennan Best</u>				
Samples Received for Transport/Shipment by:					
Samples Received for Transport/Shipment by:					
Samples Shipped Via:					
Samples Received at Laboratory by:	<u>Jeff Johnson</u>				
Samples Analyzed by:	<u>Jeff Johnson</u>				
Samples Analyzed by:					
Data Checked by:	<u>J. M.</u>				
Date:	7/2/10	Time:	1500		
Date:		Time:			
Date:		Time:			
Date:		Time:			
Date:		Time:			
Date:		Time:			
Date:		Time:			
Date:		Time:			
Date:		Time:			

CHAIN OF CUSTODY RECORD

Page 2 of 2

Job No.:	10-274	Project Manager:	Hutcherson	Method:	5B / otm 28			
Job Name:	Citgo	Project Supervisor:	Cutts					
Location:	Lemont, IL	SAMPLE ANALYSIS REQUIRED						
Unit:	FCCU WESP Stack	#	O	A R T	H C L	S O S	Recovered by	REMARKS (Specific Compounds/Methods)
			O F	C O N T	Absorb. Solution	Initial Vol.		
Run 3 cpm Filter	7/1/0	1825	1					
TB pH Filter cpm		1300	1					
TB Blt imp 1-2		1300	1					
TB Methylene wsh		1301	1					
FF								
Blank Filter		1310	1					
Blank Acetone		1315	1					
Blank methylene chloride		1316	1					
Blank DI		1317	1					
G-5								
Samples Received for Transport/Shipment by:	<i>Biology Buks</i>					Date: 7/21/0	Time: 1500	
Samples Received for Transport/Shipment by:						Date: _____	Time: _____	
Samples Received for Transport/Shipment by:						Date: _____	Time: _____	
Samples Shipped Via:						Date: _____	Time: _____	
Samples Received at Laboratory by:	<i>Randy Alderson</i>					Date: 7/22/0	Time: 0940	
Samples Analyzed by:	<i>Randy Alderson</i>					Date: 7/22/0	Time: 1400	
Samples Analyzed by:						Date: 08/10/0	Time: 1200	
Data Checked by:						Date: _____	Time: _____	





APPENDIX H

Resumes of Test Personnel



ROBERT M. PATTERSON; President

Education B. S. 1983, Central Michigan University; Mt. Pleasant, Michigan, in Geology and Earth Science-Meteorology.

Professional Training Courses Attended a two-day short course, "Performing and Observing Source Sampling" in Dallas, Texas.

Attended a one-day short course on basic supervision.

Attended a four-week management course presented by the American Management Association, 1991-1992.

Certification Certified Visible Emissions Evaluator
Certified Cabot Full-Face Respirator Fit Tester

Professional Memberships Source Evaluation Society
American Management Association

Technical Experience Participated in the sampling of over 1,000 sources, including several of which were sampled simultaneously using more than one sampling train. Thoroughly trained in all EPA testing procedures, 1986-present.

Over nineteen years experience with EPA and Texas Air Control Board methods of sampling - both stationary sources and ambient air. CFR, Title 40, Chapter I, Part 60, EPA Methods 1 through 25, and 101 through 110. Performance Specifications 1 through 5. CFR, Title 40, Chapter I, Part 50, Appendix A through F. "Sampling Procedures Manual, Texas Air Control Board, January 1983." Parts 1-1 through 14-6, Appendix B through Appendix M.

Experienced with sampling Method 0010, Modified Method 5 Sampling Train; Method 0030, Volatile Organic Sampling Train; and various EPA and "Site Specific" multiple metal and acid gas sampling trains.

(continued)
H-2

10-274B



PATTERSON, Rob (cont'd)

Technical
Experience
(cont'd)

Over twenty one years experience with EPA and Texas Air Control Board methods of analysis of both stationary and ambient air samples. Particulate matter, SO₃, SO₂, H₂SO₄, NO_x, CO, CO₂, O₂, H₂S, F, TRS, HCl, Cl₂, NH₃, VOC, C₁-C₇, and other organics. Both laboratory and on-site analyses were performed.

Experienced in the sampling and analysis of commercial calibration gas cylinders for sulfur dioxide, oxides of nitrogen, carbon dioxide, oxygen, carbon monoxide, and C₁-C₇ hydrocarbons.

Thoroughly trained in the operation and routine maintenance of the following:

- MSA LIRA Model 202S Infrared Analyzer
- Analytical Instrument Development, Inc. Model 340A Calibration System
- Shimadzu GC-Mini 2 Gas Chromatograph
- Thermo Environmental Model 10AR Oxides of Nitrogen Analyzer
- Thermo Oxygen Analyzer
- Teledyne Model 326 Oxygen Analyzer
- Thermo Environmental Model 48 Carbon Monoxide Analyzer
- Thermo Environmental Model 40 Sulfur Dioxide Analyzer
- Ratfisch Model RS 100 Total Hydrocarbon Analyzer
- Western Research Model 721AT Sulfur Dioxide Analyzer
- Horiba Model PIR 2000 Carbon Dioxide Analyzer
- Ratfisch Model RS 55 Total Hydrocarbon Analyzer
- J.U.M. Model VE-7 Total Hydrocarbon Analyzer



JAMES R. MONFRIES; Senior Quality Assurance Manager

Education B. S. 1975, University of Texas at Arlington; Arlington, Texas, in Biology with a minor in Chemistry.

Graduate work at the University of Texas at Dallas in the Environmental Science Department.

Professional Training Courses Attended a two-day short course, "Performing and Observing Source Sampling" in Dallas, Texas, July 1976.

Certification Qualified Individual (Groups I, II, III, and IV)
Certified Visible Emissions Evaluator

Professional Memberships Air and Waste Management Association
Source Evaluation Society - Past President

Technical Experience Participated in the sampling of over 700 sources, serving in the supervisory capacity on over 500 sources. Many of the sources were sampled simultaneously using more than one sampling train at several points in the flue gas stream, 1976-present.

Also supervised several ambient air monitoring studies, including a permanent five-station high volume air sampling network in South Texas, a permanent four-station high volume air sampling network in Pennsylvania, and a permanent seven-station sulfur dioxide sampling network in East Texas.

Was Quality Assurance Manager for several ambient air monitoring studies; including a four-station high volume air sampling network for TSP and PM10 in Midlothian, Texas; a single-station high volume air sampling network for PM10 in South Texas, a two-station high volume air sampling network for TSP in Wichita Falls, Texas, and a four-station continuous air sampling network for TSP and PM10 in Jewett, Texas using Thermo Andersen FH 62 C14 Beta Gauge Dust Monitors.



MONFRIES, James (cont'd)

Thirty years experience with EPA and Texas Commission on Environmental Quality methods of analysis of both source and ambient air samples for particulates, SO₂, SO₃, H₂SO₄, H₂S, HCl, Cl₂, NO_x, Hydrocarbons, and TRS.

Experienced in the analysis of commercial calibration gas cylinders for sulfur dioxide and oxides of nitrogen.

Experienced with VOST and Modified Method 5 Sampling Procedures.

Thoroughly trained in the operation and routine maintenance of the following:

- Lear Siegler, Inc. SM800 Stack Gas Monitor
- Du Pont Model 460/1 Photometric Analyzer System
- Lear Siegler, Inc. SM1000 Ambient SO₂ Monitor
- Calibrated Instruments Ultragas SO₂ Monitor
- Meloy 285E SO₂ Analyzer
- Meloy SA-700 Fluorescent SO₂ Analyzer
- MSA LIRA Model 202S Infrared Analyzer
- Analytical Instrument Development, Inc.
Model 340A Calibration System
- Shimadzu GC-Mini 2 Gas Chromatograph
- Thermo Environmental Model 10S NO_x Analyzer
- Thermo Oxygen Analyzer
- Teledyne Model 326 Oxygen Analyzer
- Thermo Environmental Model 48 Carbon Monoxide Analyzer
- Thermo Environmental Model 40 Sulfur Dioxide Analyzer
- Ratfisch Model RS 103 Total Hydrocarbon Analyzer
- Western Research Model 721AT Sulfur Dioxide Analyzer
- Horiba Model PIR 2000 Carbon Dioxide Analyzer
- Ratfisch Model RS 55 Total Hydrocarbon Analyzer
- J.U.M. Model VE-7 Total Hydrocarbon Analyzer
- Thermo Andersen Model FH 62 C14 Dust Monitor



JOHN CUTAIA; Project Supervisor

Education

Over ten (10) years of experience using Methods 1, 2, 3, 4, 5, 6, 7, 9, 10, 11, 24, 29, 201A.

Analyzers used: Thermo 43A, 51, 48C, 42C, Servomex 1400, 1400C; Fuj. 3300, Horiba VIA-510, Western 721, Rosemont 951A

Technical Experience

Participated in the sampling of over 150 sources, including several of which were sampled simultaneously using more than one sampling train.

Thoroughly trained in all EPA testing procedures, 2005-present.



KYLE GILBERT; Environmental Scientist III

Education B. S. in Biology, August 2007; Stephen F. Austin State University,
 Nacogdoches, Texas.

Technical
Experience Participated in the sampling of over 100 sources, including
 several of which were sampled simultaneously using more
 than one sampling train.

Thoroughly trained in all EPA testing procedures, 2007-present.



SAMUEL A. MORRIS; Environmental Scientist II

Education B.S. (Biological Sciences) May 2007, Louisiana State University;
 Baton Rouge, Louisiana.

Technical
Experience Participated in the sampling of over 50 sources, including
 several of which were sampled simultaneously using more
 than one sampling train.

Thoroughly trained in all EPA testing procedures, 2008-present.



WILLIAM W. STARKEY; Environmental Scientist II

Education Computer Science, May 2003 – Albany, Louisiana.
1-1/2 years of testing experience

Technical Experience Participated in the sampling of over 50 sources, including several of which were sampled simultaneously using more than one sampling train.

Thoroughly trained in all EPA testing procedures, 2007-present.



BIPPERT, Landon; Environmental Scientist I

Education Bio Environmental Science, December 2008; Texas A&M University, College Station, Texas.

Technical Experience Participated in the sampling of over 25 sources, including several of which were sampled simultaneously using more than one sampling train.

Thoroughly trained in all EPA testing procedures, 2009-present.